

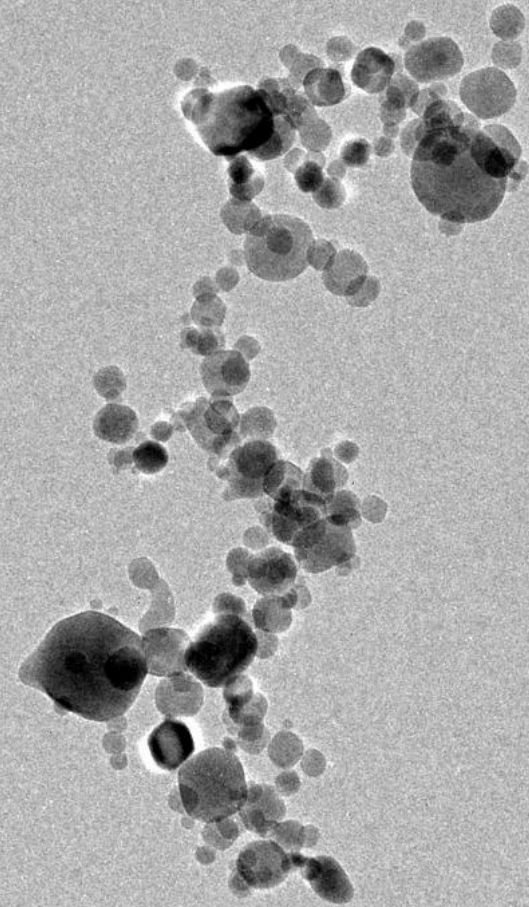
# Dynamics of Fractal-like Aerosols during Sintering: Characterization

Max L. Eggersdorfer and Sotiris E. Pratsinis  
Particle Technology Laboratory, ETH Zürich



# Our motivation: Characterization of nanoparticle structure during gas-phase synthesis

- formation of agglomerates & aggregates

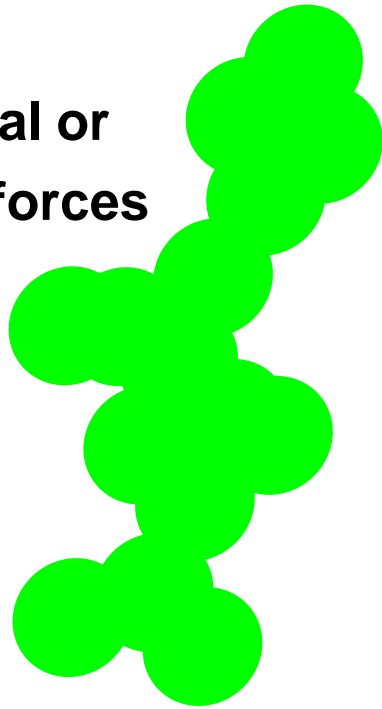
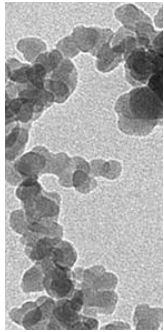


100 nm



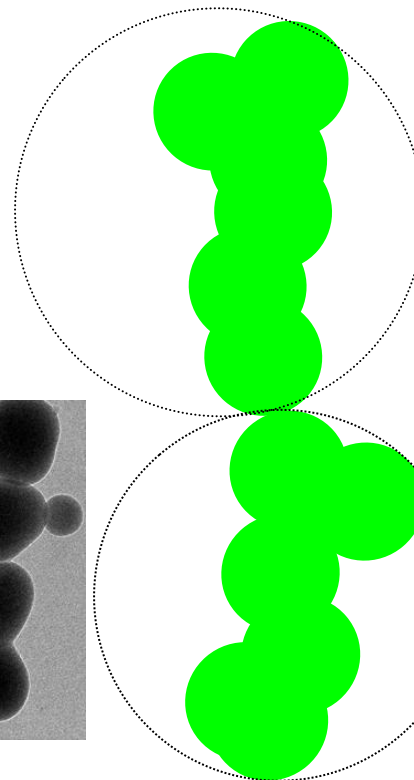
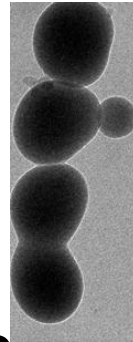
# Aggregates and Agglomerates

Chemical or  
Sinter-forces



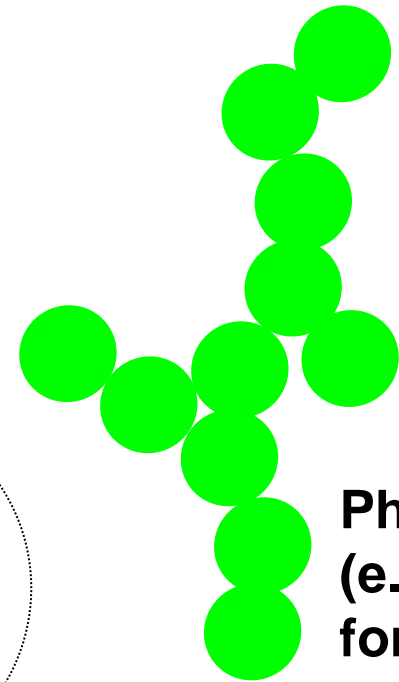
Catalysts, lightguides,  
devices

Less toxic?

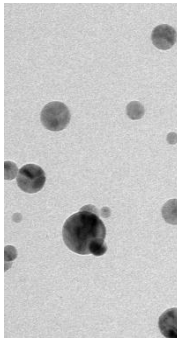


Nanocomposites, paints

Potentially toxic?

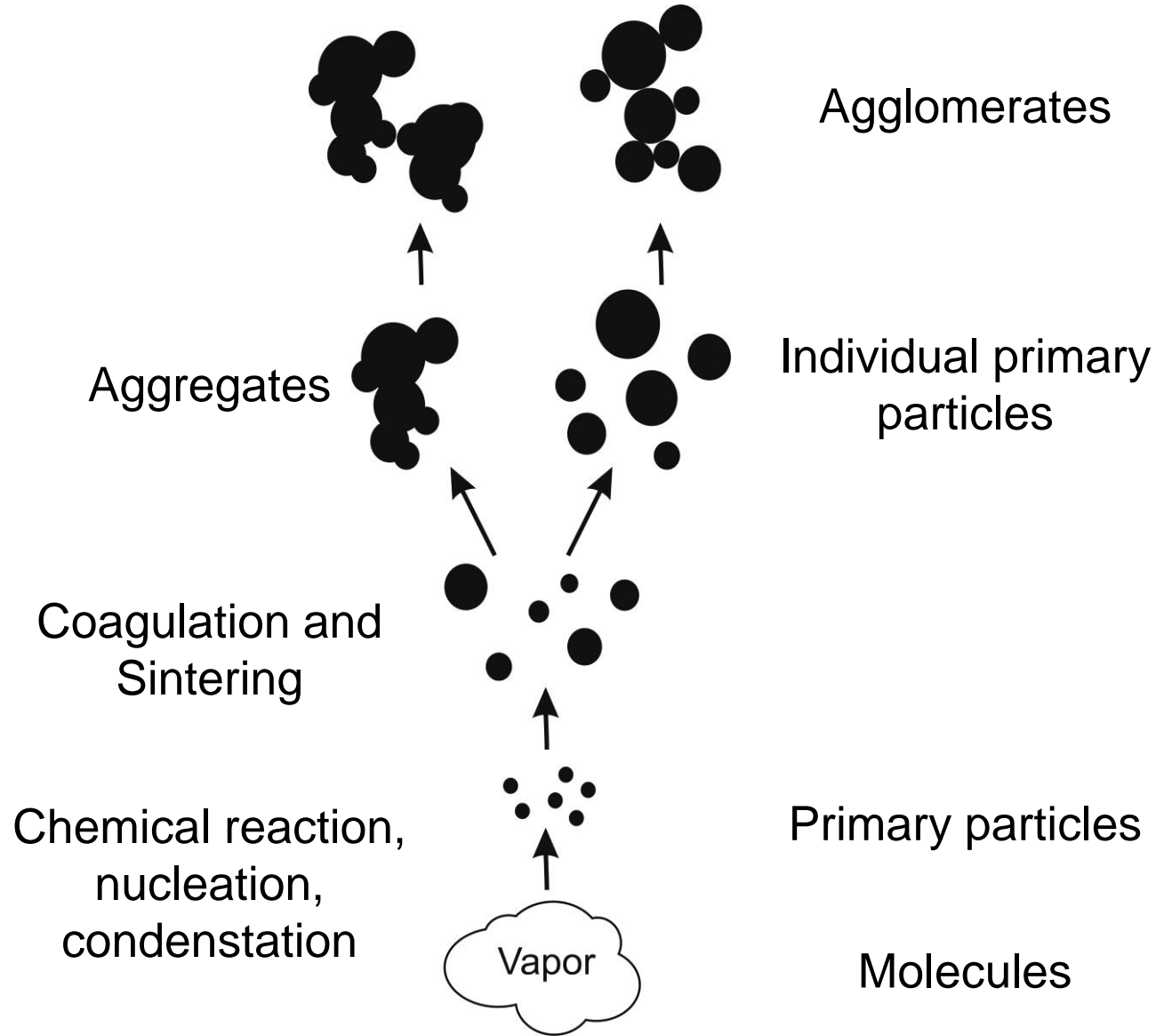
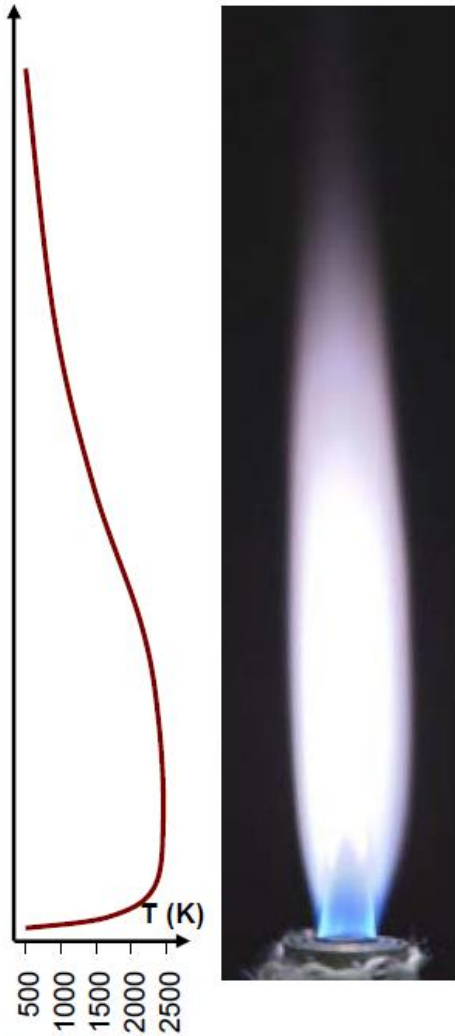


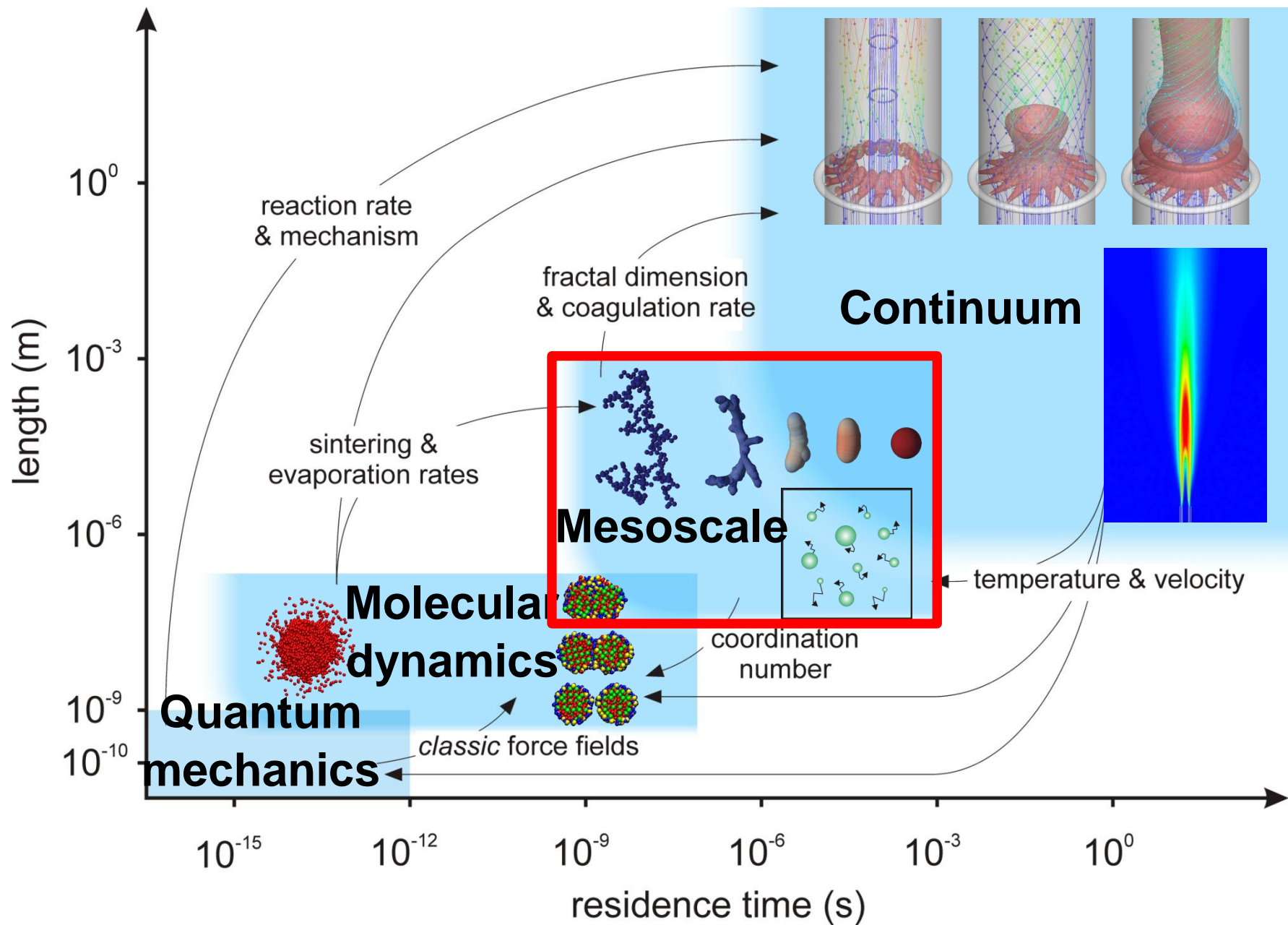
Physical  
(e.g.vdW)  
forces



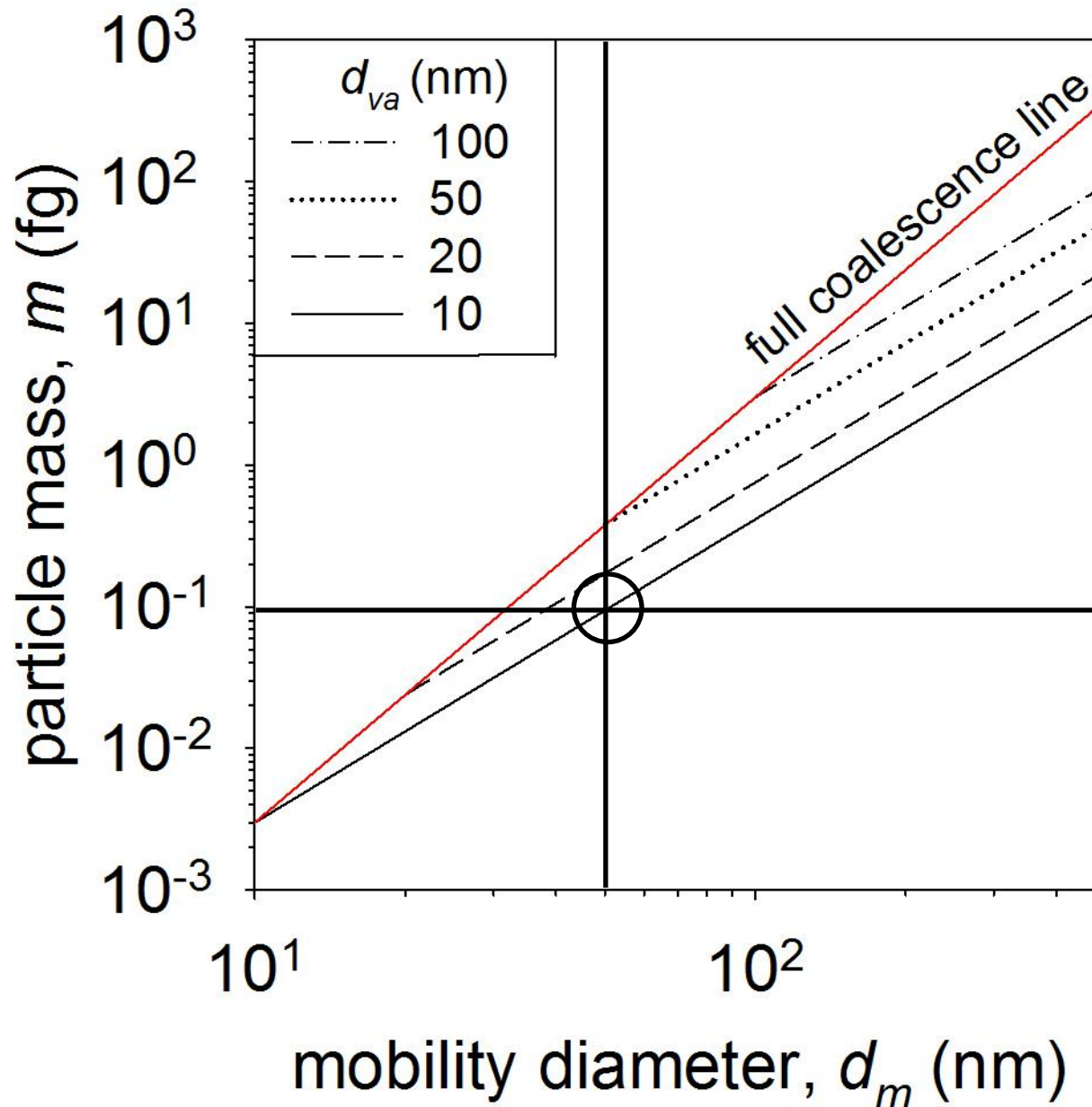
Current aerosol instruments cannot distinguish them

# Particle Generation in the Gas-Phase





# Relation between mass, mobility and primary diameter



measure:

$$d_m = 50 \text{ nm}$$

$$m = 9 \cdot 10^{-2} \text{ fg}$$

calculate:

$$d_{va} = 10 \text{ nm}$$

$$\rho = 5720 \text{ kg/m}^3$$

## Part 1: Numerical

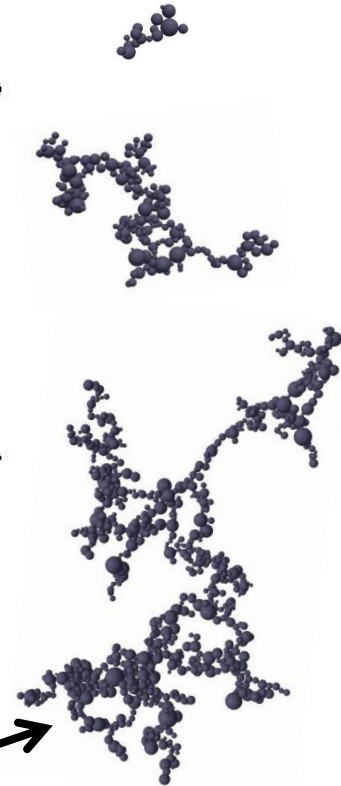
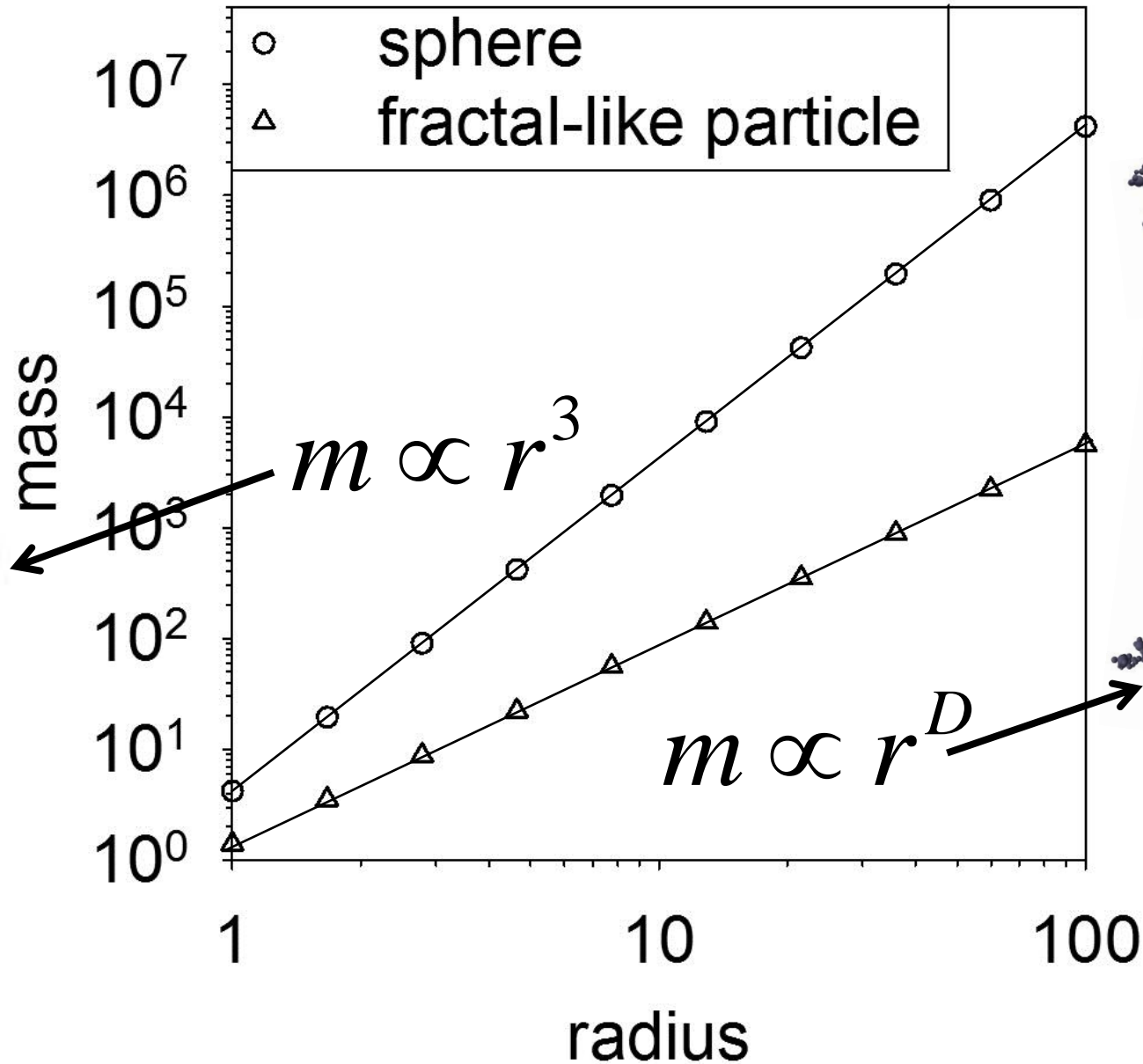
- characterization of agglomerate structure
- formation of aggregates by sintering

**→ mass – mobility relation**

## Part 2: Experimental

- mass-mobility characterization of  $\text{ZrO}_2$

# Scaling of Agglomerate Structure





# Characteristic Agglomerate Radius



Mass fractal dimension<sup>1</sup>,  $D_f$

$$\frac{m}{m_p} = k_n \left( \frac{r_g}{r_p} \right)^{D_f}$$

Mass-mobility exponent<sup>3</sup>,  $D_{fm}$

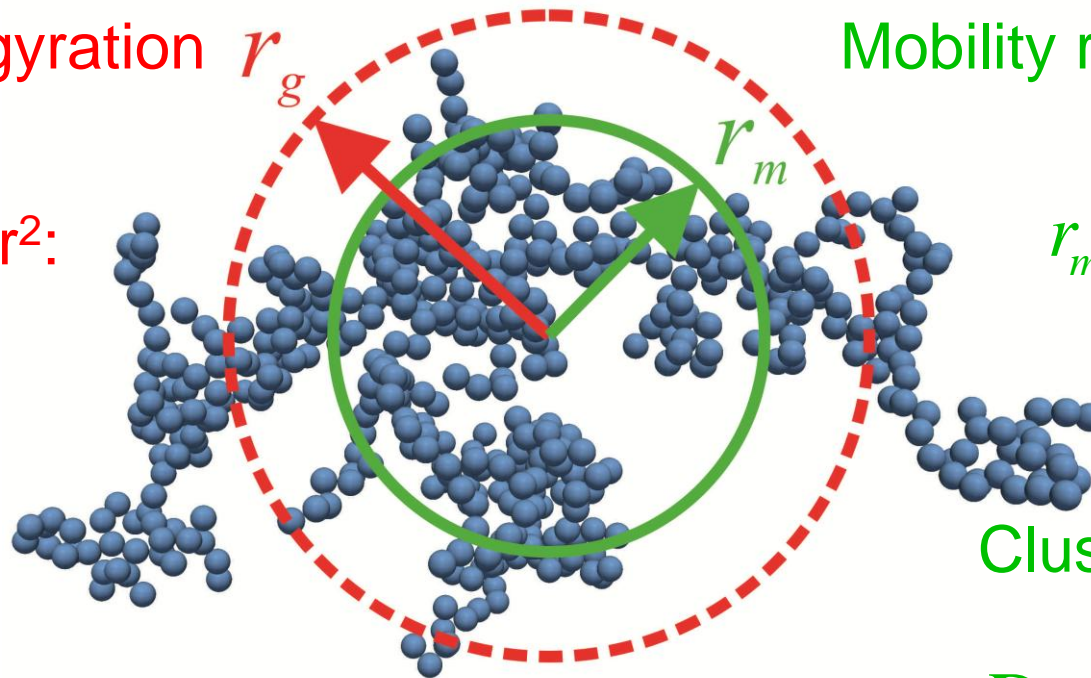
$$\frac{m}{m_p} = k_m \left( \frac{r_m}{r_p} \right)^{D_{fm}}$$

Radius of gyration  $r_g$

Mobility radius

Cluster-cluster<sup>2</sup>:

$$D_f \approx 1.8$$



$$r_m = \sqrt{\frac{a_a}{\pi}}$$

Cluster-cluster<sup>2</sup>:

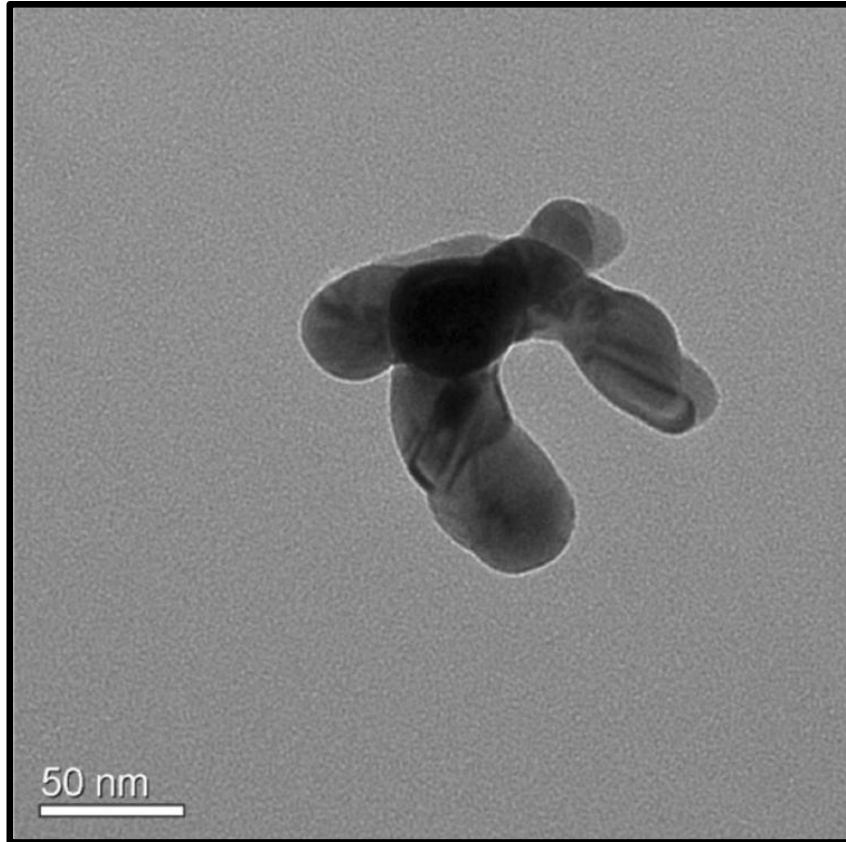
$$D_{fm} \approx 2.15$$

1. S.R. Forrest & T. A. Witten, *J. Phys. A: Math. Gen.* **12** (1979) L109-L117.
2. C.M. Sorensen, *Aerosol Sci. Technol.* **45** (2011) 755-769.
3. K. Park, F. Cao, D.B. Kittelson & P.H. McMurry, *Environ. Sci. Technol.* **37** (2003), 577-583.

# Formation of Aggregates by Sintering

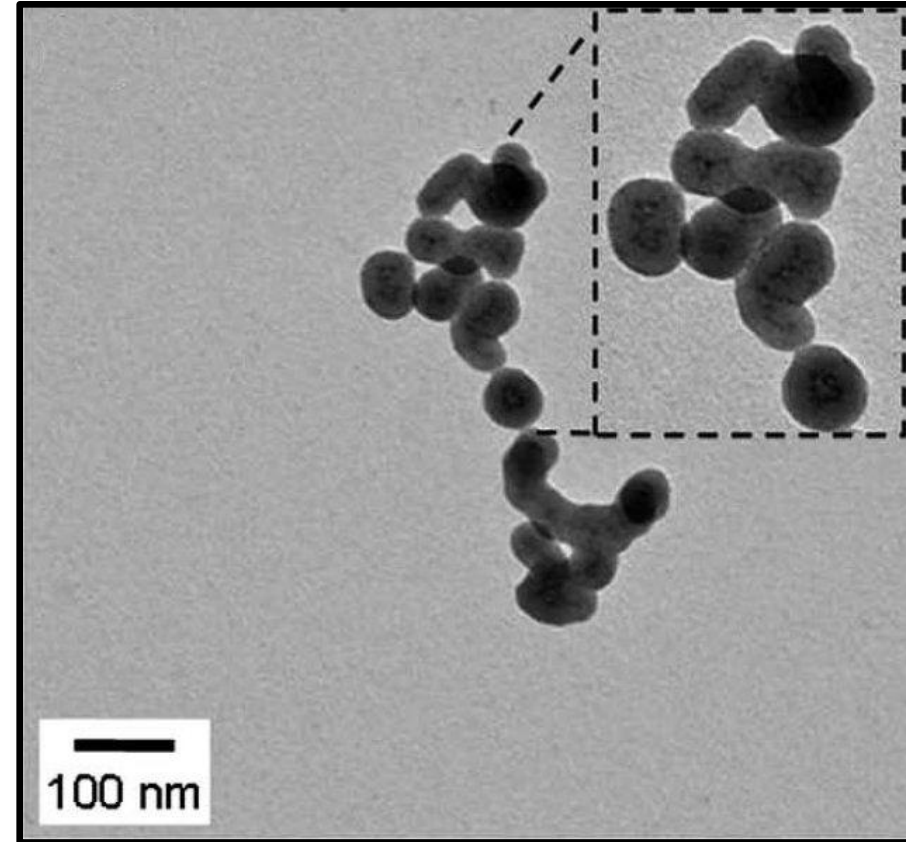


Ag: grain boundary diffusion



S.C. Kim, J. Wang, M.S. Emery, W.G. Shin, G.W. Mulholland & D.Y.H. Pui, *J. Aerosol Sci.* **43** (2009) 344-355.

SiO<sub>2</sub>: viscous flow sintering



J.C. Park, D.A. Gilbert, K. Liu & A.Y. Louie, *J. Mater. Chem.* **22** (2012) 8449-8454.

# Simulation Method: Viscous Flow Sintering



## Geometric Model

1. Energy balance<sup>1</sup>

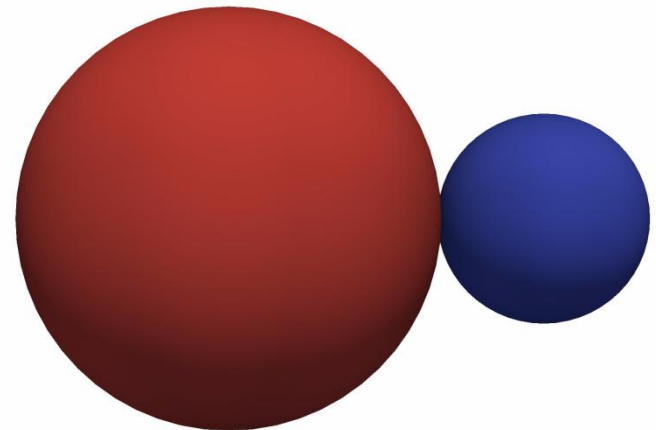
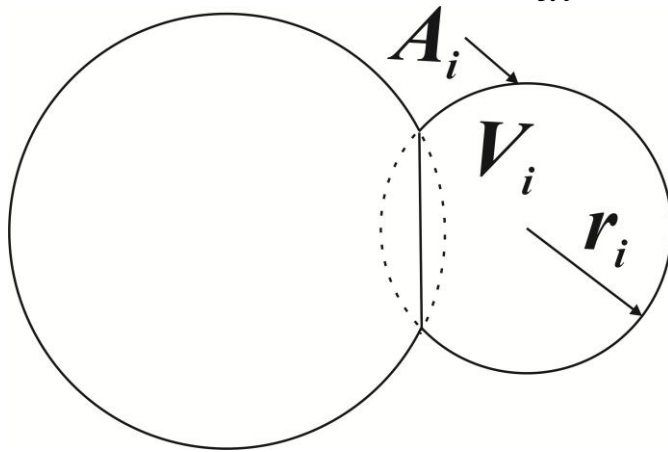
$$\underbrace{\gamma \frac{dA_i}{dt}}_{\text{Change in surface energy}} = \underbrace{\iiint 3\eta \dot{\epsilon}^2 dV_i}_{\text{viscous dissipation}} = 3\eta \dot{\epsilon}^2 V_i$$

Constant strain rate  $\dot{\epsilon}$  in particle

Change in surface energy = viscous dissipation

2. Mass balance<sup>2</sup>

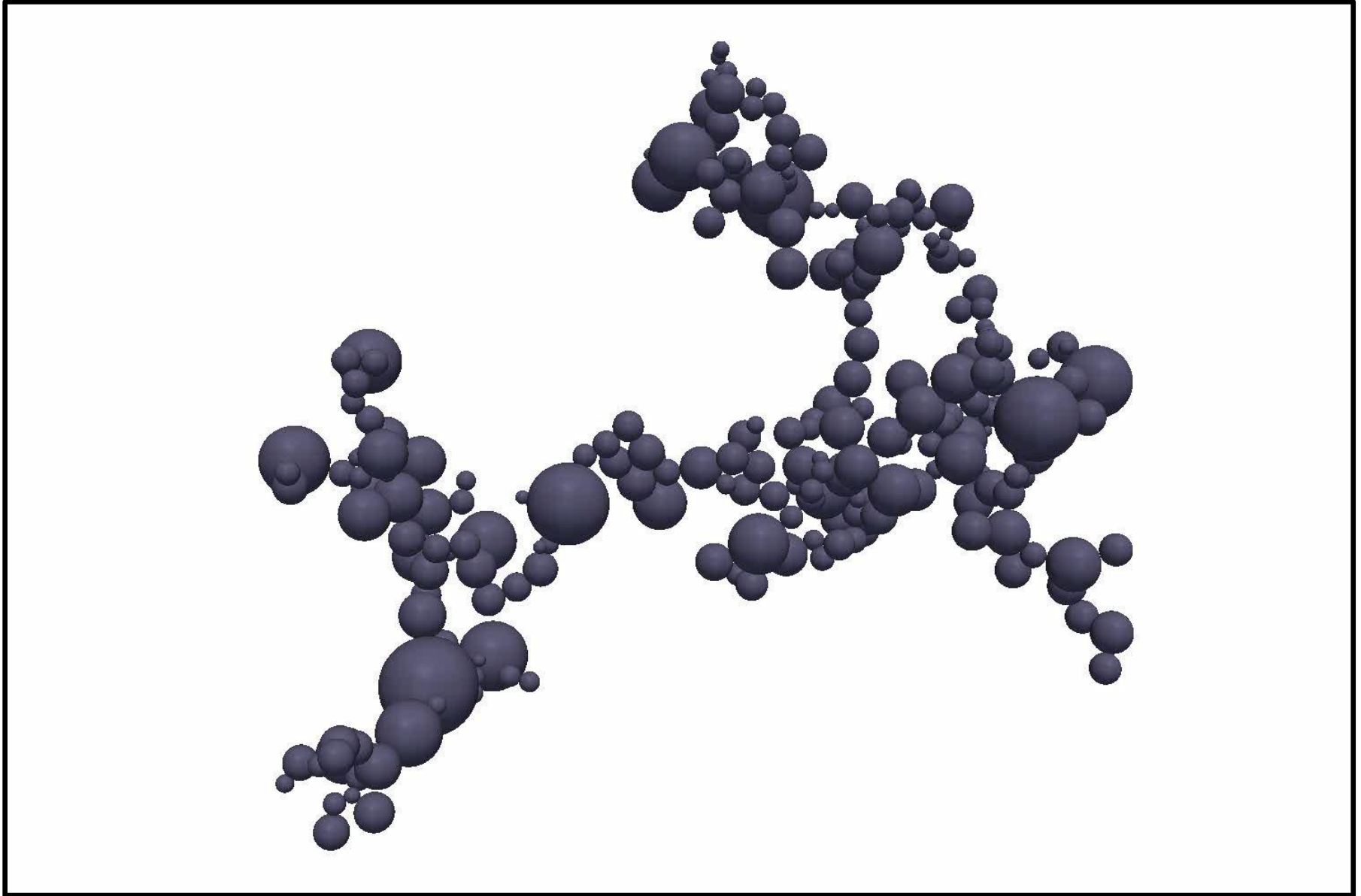
$$\frac{dV_i}{dt} = 0$$



1. J. Frenkel, *J. Phys.* **9** (1945) 385-391.

2. R.M. Kadushnikov, V.V. Skorokhod, I.G. Kamenin, V.M. Alievskii, E.Y. Nurkanov, D.M. Alievskii, *Powder Metall. Met. C+* **40** (2001) 154-163.

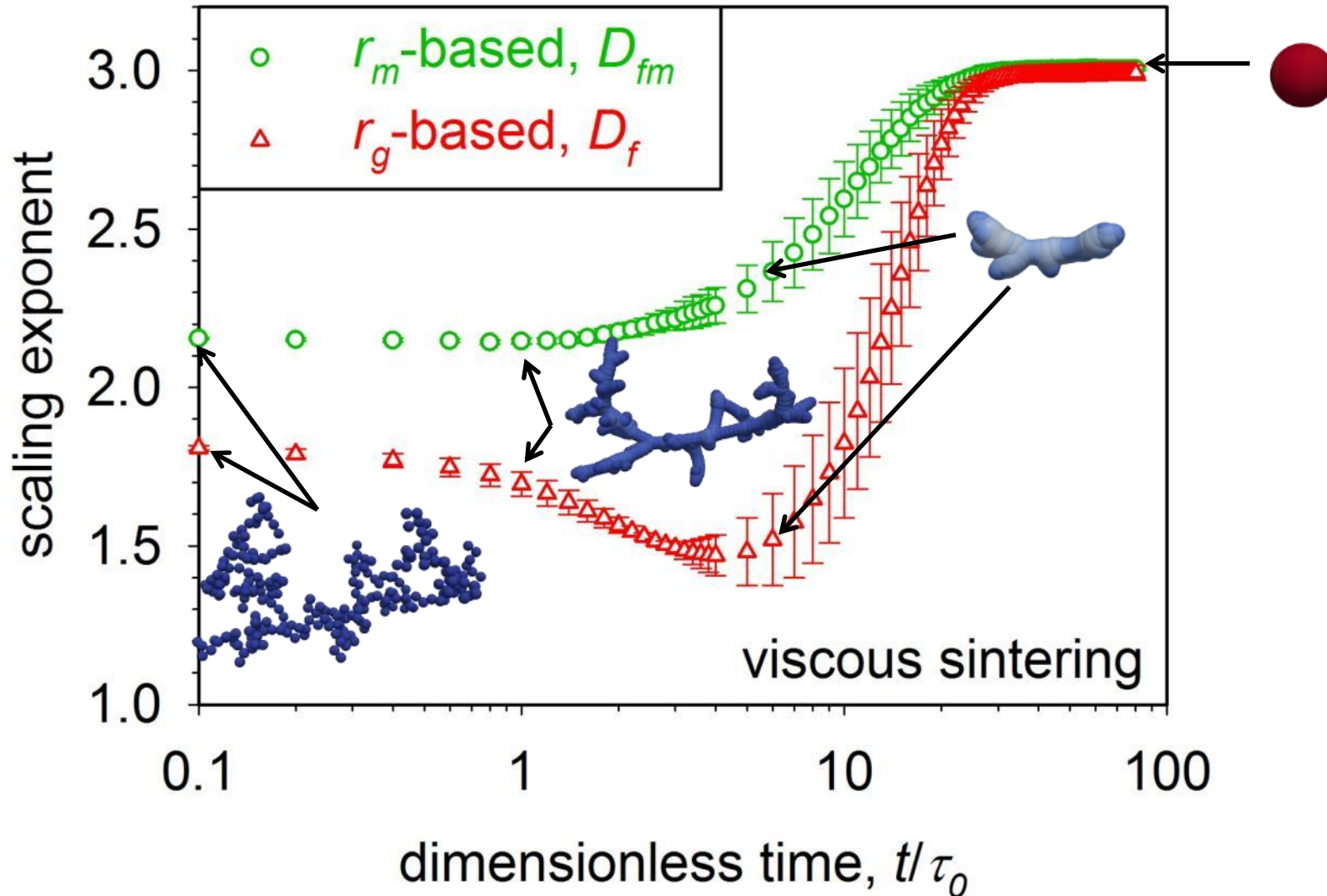
# Formation of Aggregates by Sintering



# Evolution of $D_f$ & $D_{fm}$



Ensemble average over 200 clusters with 16-512 PPs



1. A. Camenzind, H. Schulz, A. Teleki, G. Beaucage, T. Narayanan & S.E. Pratsinis, *Eur. J. Inorg. Chem.* (2008) 911-918.

# Scaling of Projected Aggregate<sup>1</sup> Area during Sintering

$$n_{va} = k_a \left( \frac{a_a}{a_{va}} \right)^{D_\alpha}$$

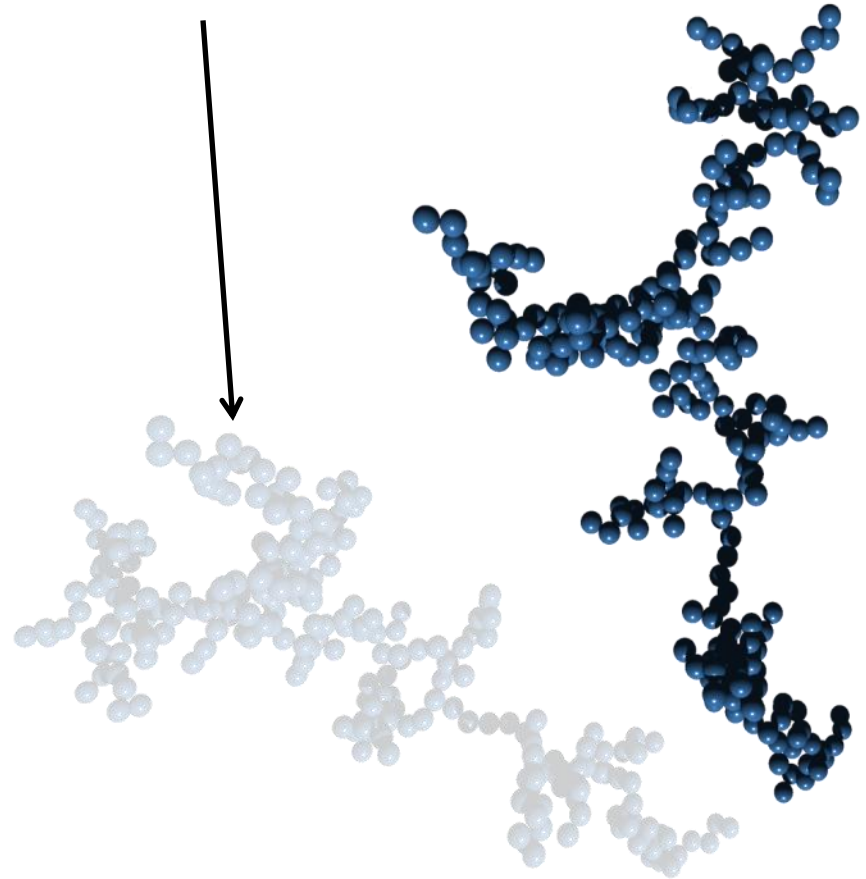
$a_a$ : projected area

$d_{va}$ : average PP diameter

$$d_{va} = d_{BET} = \frac{6v}{a}$$

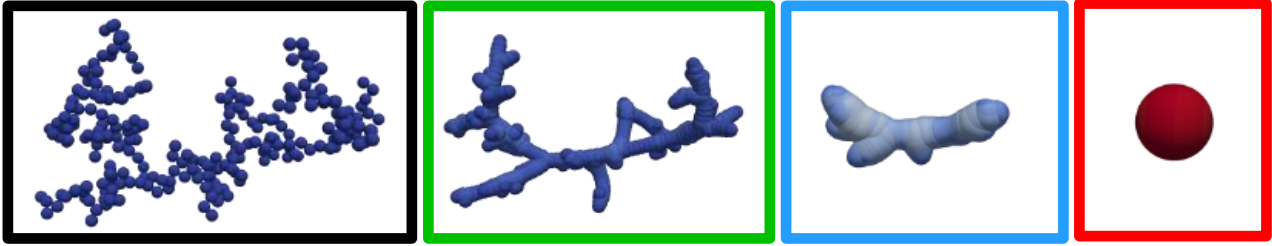
$n_{va}$ : average number of PPs

$$n_{va} = \frac{v}{\pi d_{va}^3 / 6}$$



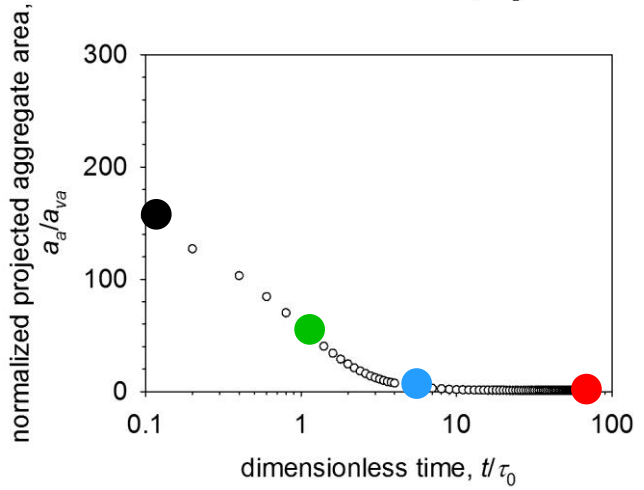
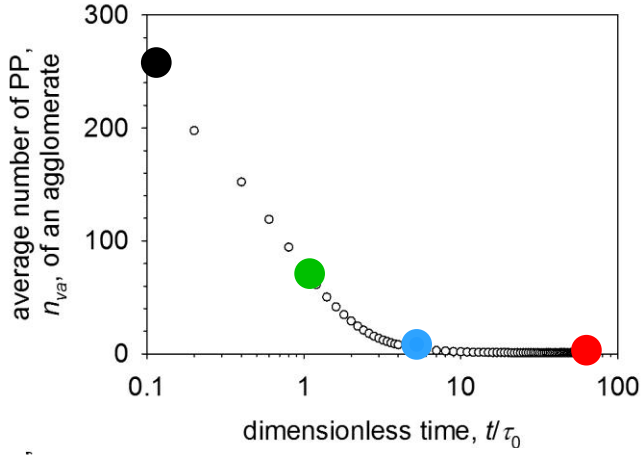
1. A.I. Medalia, *J. Colloid Interface Sci.* **24** (1967) 393-404.

# Scaling of Projected Aggregate<sup>1</sup> Area during Sintering

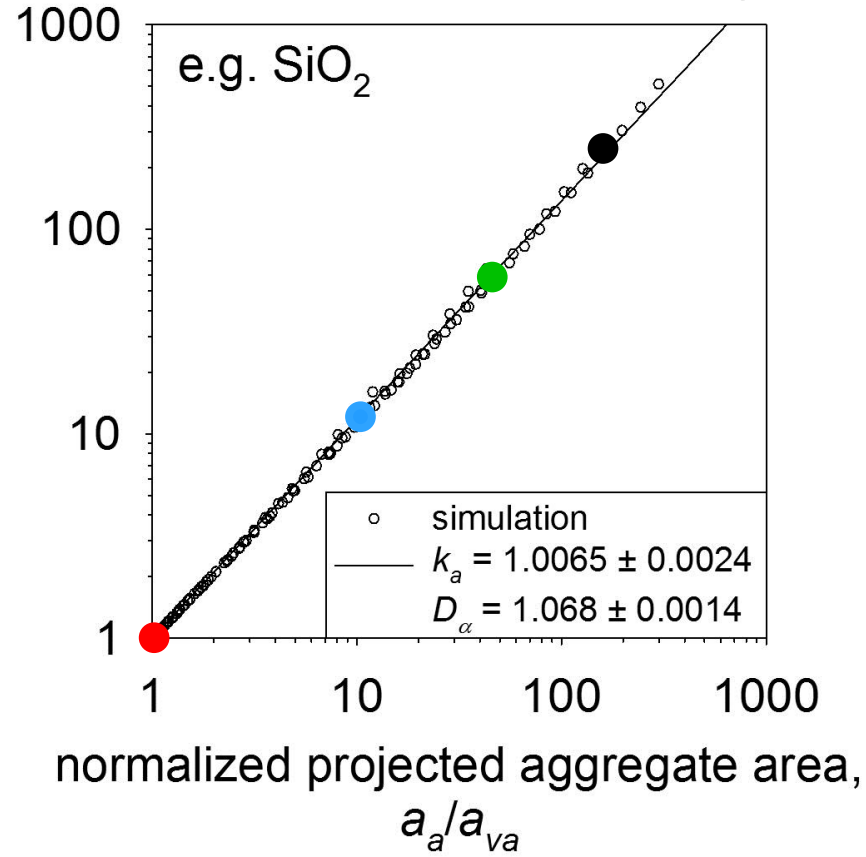


$$n_{va} = k_a \left( \frac{a_a}{a_{va}} \right)^{D_\alpha}$$

viscous flow sintering<sup>2</sup>



average number of PP,  $n_{va}$  of an aggregate



1. A.I. Medalia, *J. Colloid Interface Sci.* **24** (1967) 393-404.

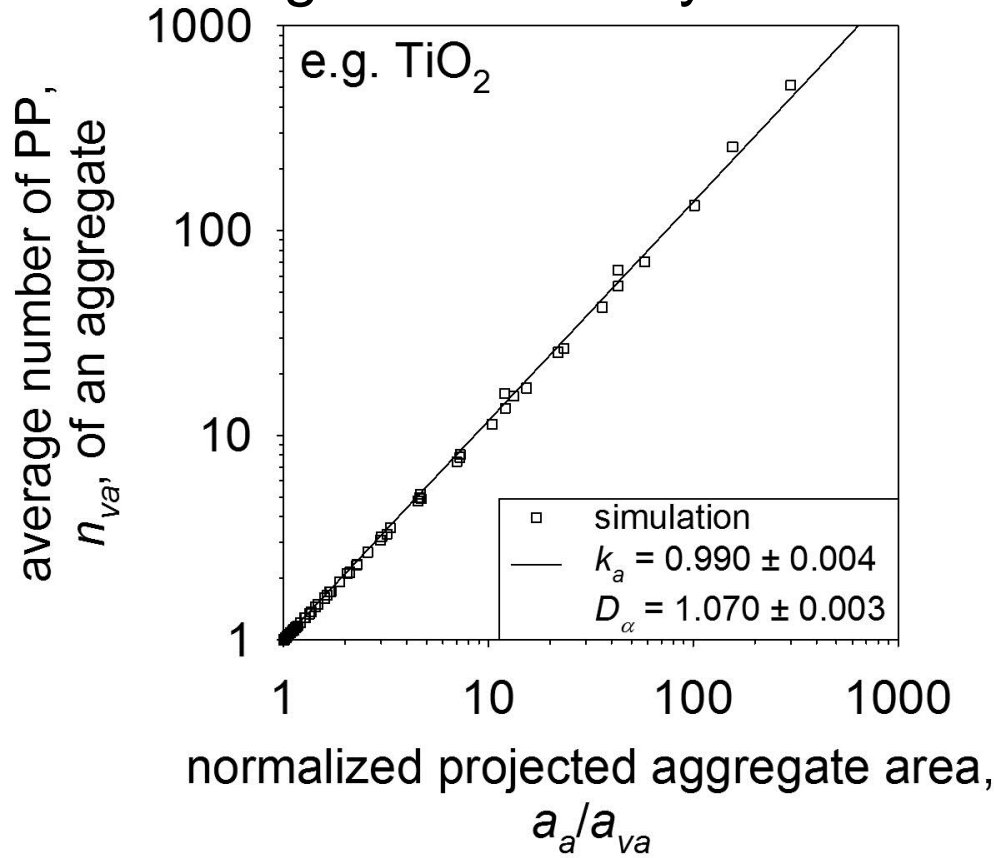
2. M.L. Eggersdorfer, D. Kadau, H.J. Herrmann & S.E. Pratsinis, *Langmuir* **27** (2011) 6358-6367.

# Scaling of Projected Aggregate<sup>1</sup> Area during Sintering

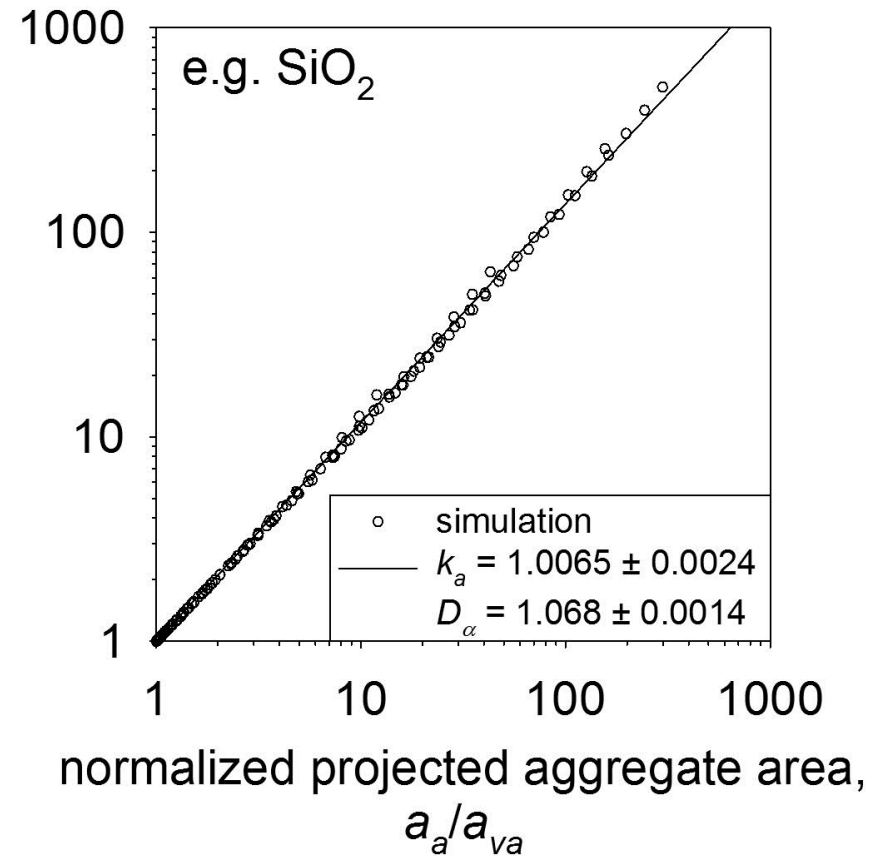
$k_a = 1$  &  $D_\alpha = 1.07$  are nearly independent of sintering mechanism

$$n_{va} = k_a \left( \frac{a_a}{a_{va}} \right)^{D_\alpha}$$

grain boundary diffusion<sup>3</sup>



viscous flow sintering<sup>2</sup>



1. A.I. Medalia, *J. Colloid Interface Sci.* **24** (1967) 393-404.

2. M.L. Eggersdorfer, D. Kadau, H.J. Herrmann & S.E. Pratsinis, *Langmuir* **27** (2011) 6358-6367.

3. M.L. Eggersdorfer, D. Kadau, H.J. Herrmann & S.E. Pratsinis, *J. Aerosol Sci.* **46** (2012) 7-19.



# Mass-mobility Relation

Surface area  
mean diameter:  $d_{va} = \frac{6v}{a}$

Average number of  
primary particles:  $n_{va} = \frac{v}{v_{va}}$

Scaling of projected  
aggregate area:<sup>1</sup>

$$n_{va} = k_a \left( \frac{a_a}{a_p} \right)^{D_\alpha}$$

$a_a$  = projected  
aggregate area

Mobility in free  
molecular<sup>2</sup> and  
transition regime:<sup>3</sup>

$$d_m = \sqrt{\frac{4a_a}{\pi}}$$

Surface area mean diameter from mobility size and volume

$$d_{va} = \left( \frac{\pi k_a}{6v} (d_m)^{2D_\alpha} \right)^{1/(2D_\alpha - 3)}$$

1. A.I. Medalia, *J. Colloid Interface Sci.* **24** (1967) 393-404.

2. P. Meakin, *Adv. Colloid Interface Sci.* **28** (1988) 249-331.

3. S.N. Rogak, R.C. Flagan & H.V. Nguyen, *Aerosol Sci. Technol.* **18** (1993) 25-47.

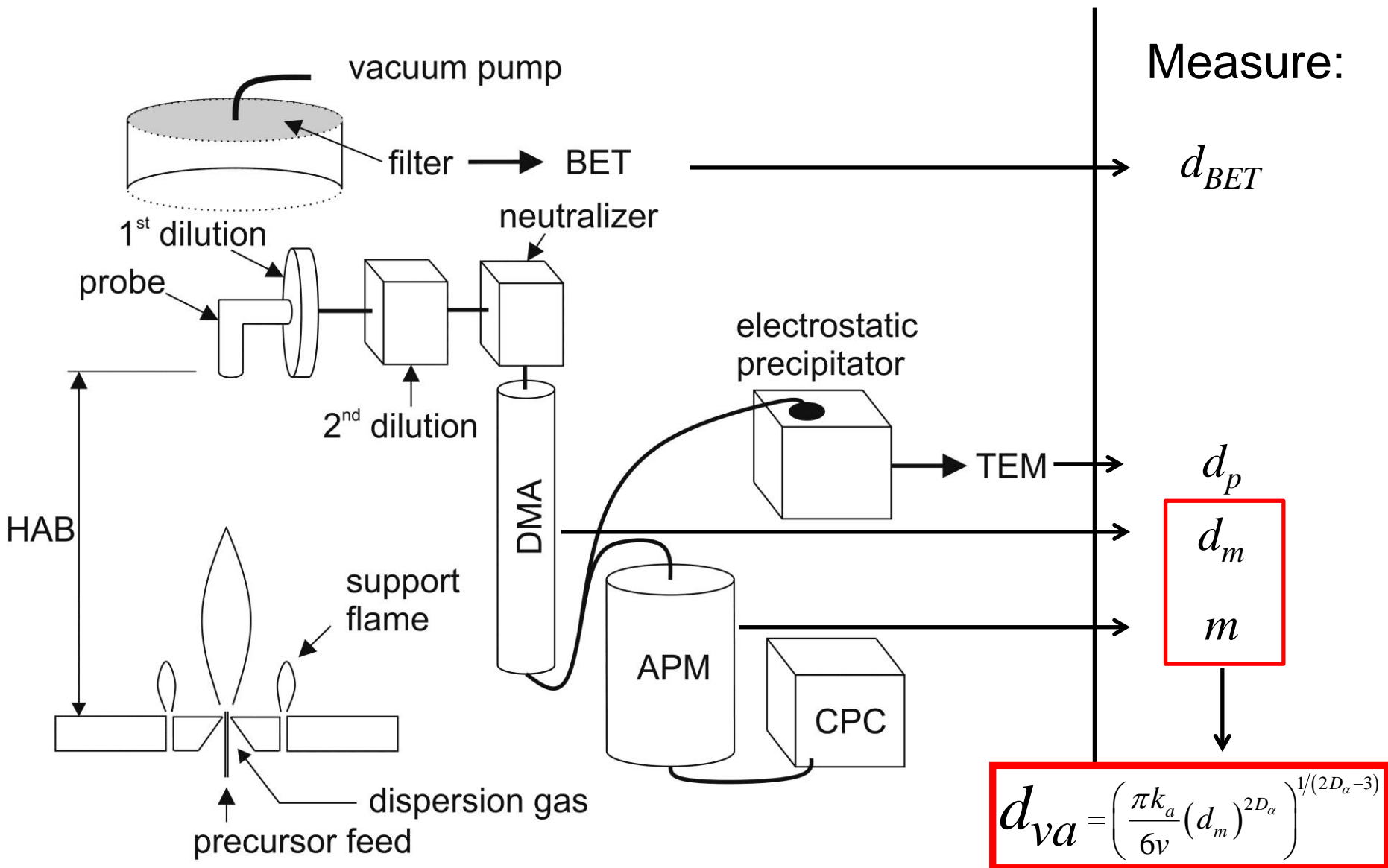
# Summary & Conclusions

- Mass-mobility relation in free molecular and transition regime:

$$d_{va} = \left( \frac{\pi k_a}{6\nu} (d_m)^{2D_\alpha} \right)^{1/(2D_\alpha - 3)}$$

- independent of time, material or sintering mechanism, with  $k_a = 1.0$  &  $D_\alpha = 1.07$

# Reality Check: Characterization of ZrO<sub>2</sub> Nanoparticles



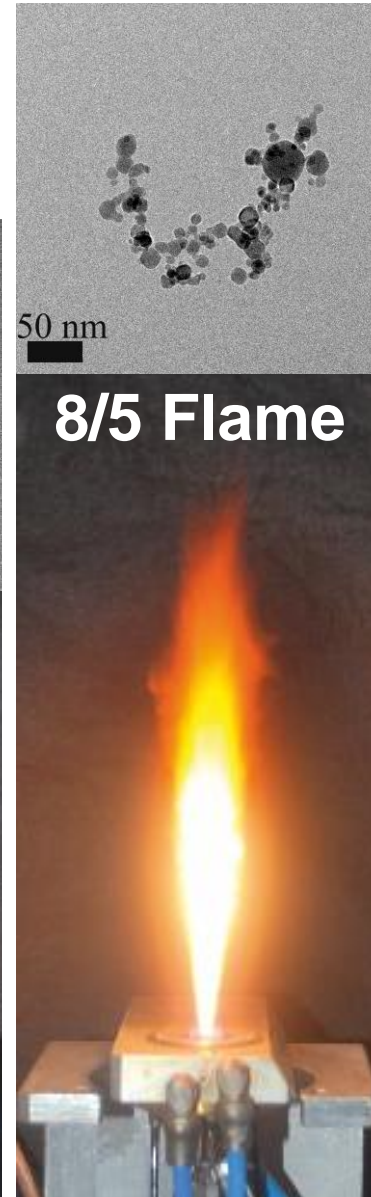
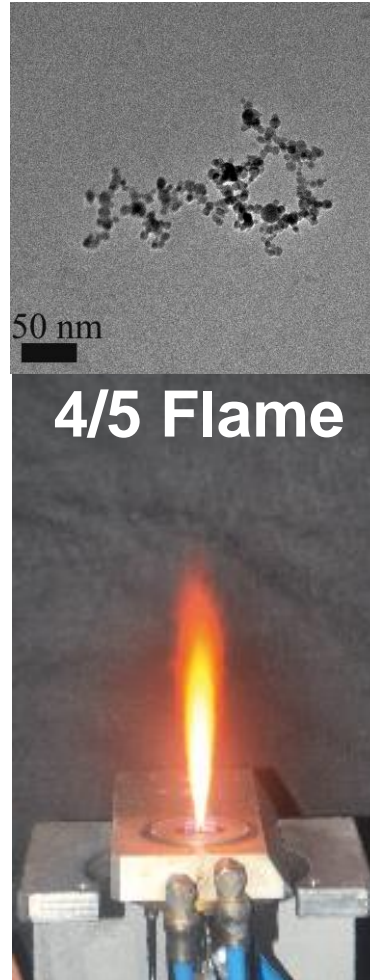
# Effect of Liquid Precursor Feed Rate X

X/Y Flame

X: precursor feed liquid (ml/min)

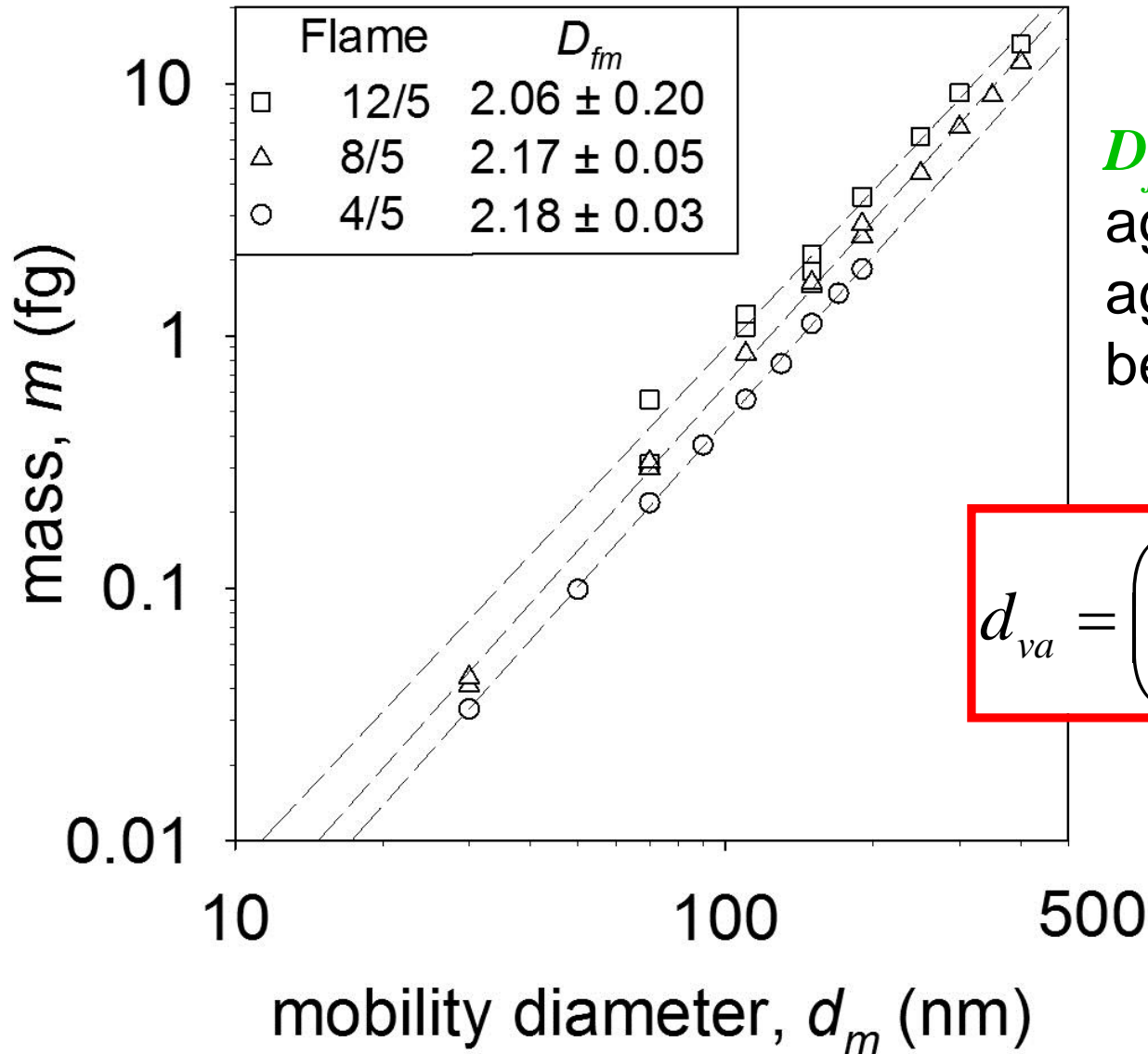
Y: dispersion gas (l/min)

Increasing liquid precursor feed rate results in faster sintering & coagulation <sup>1</sup>



1. S.E. Pratsinis, W.H. Zhu & S. Vemury, Powder Technol. 86 (1996) 87-93.

# Effect of Precursor Feed Rate: Mass-Mobility



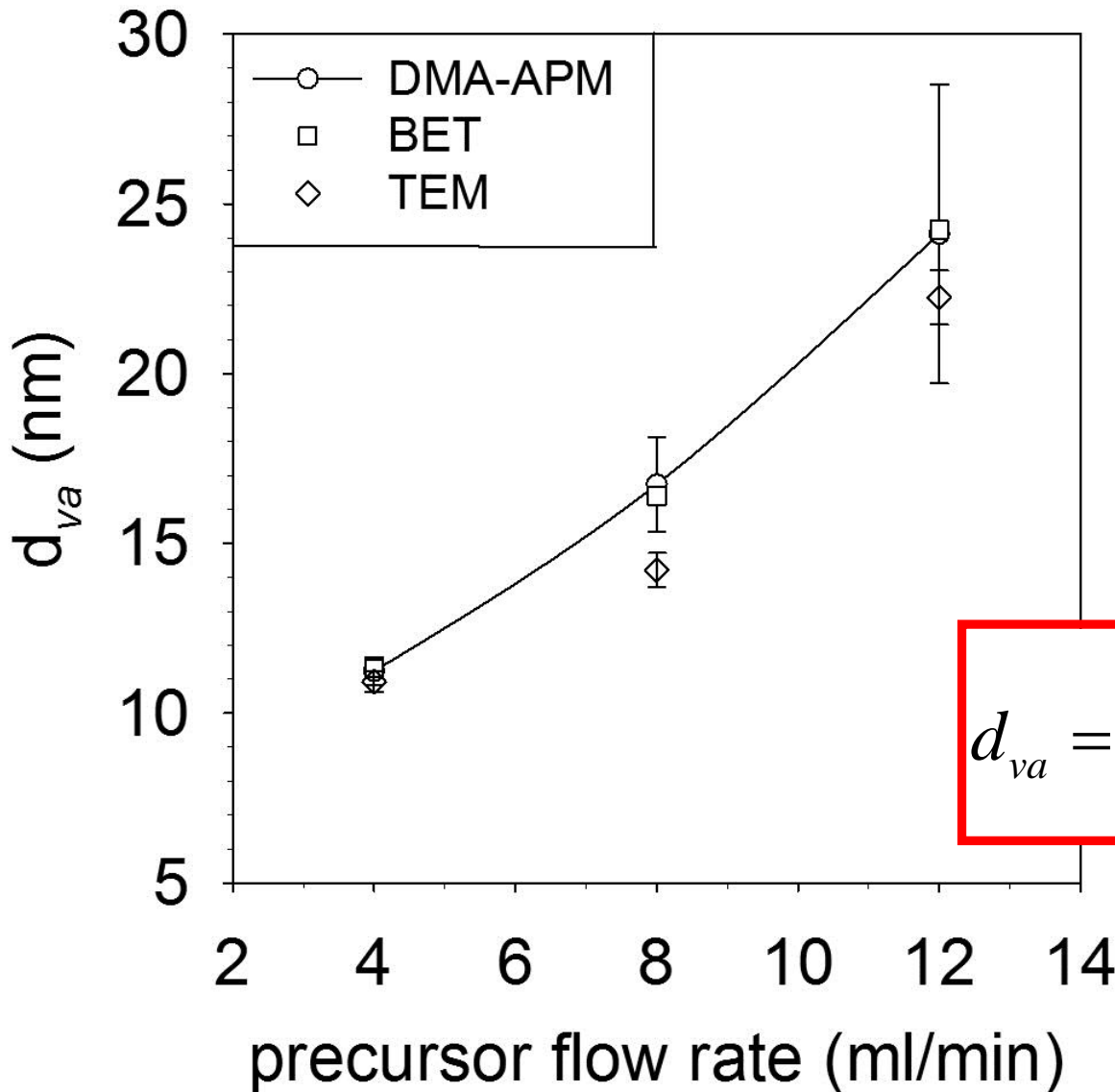
$D_{fm} \approx 2.15$ :  
agglomerates or  
aggregates at  
beginning of sintering

$$d_{va} = \left( \frac{\pi k_a}{6\nu} (d_m)^{2D_\alpha} \right)^{1/(2D_\alpha - 3)}$$

# Effect of Liquid Precursor Feed Rate: $d_{va}$



surface area mean PP diameter,  $d_{va}$  (nm)

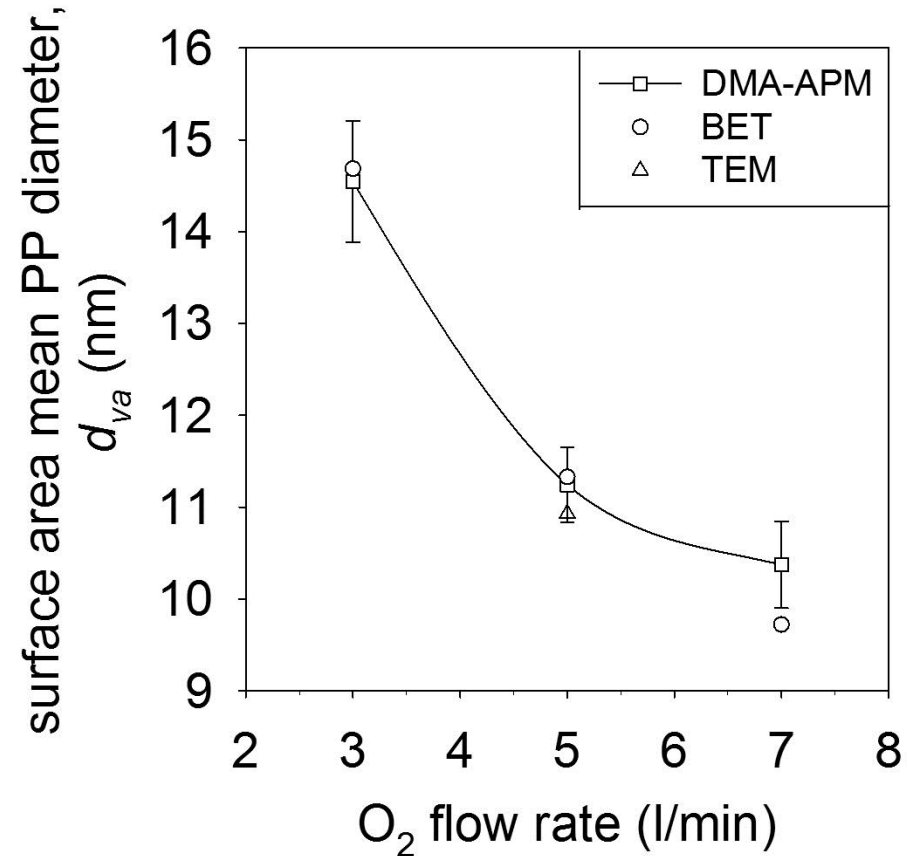
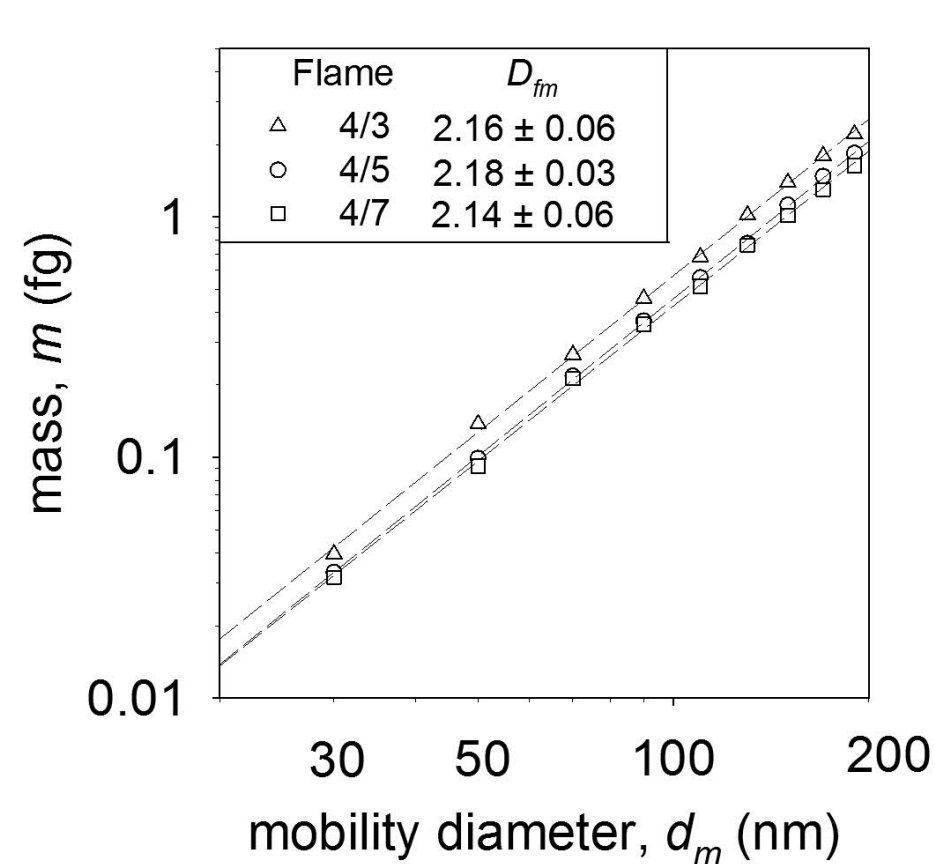


$d_{va}$  can be rapidly determined during nanoparticle production by DMA-APM measurements with material density and

$$d_{va} = \left( \frac{\pi k_a}{6v} (d_m)^{2D_\alpha} \right)^{1/(2D_\alpha - 3)}$$

M.L. Eggersdorfer, A.J. Gröhn, C.M. Sorensen, P.H. McMurry & S.E. Pratsinis, Mass-Mobility Characterization of Flame-made ZrO<sub>2</sub> Aerosols: the Primary Particle Diameter & extent of Aggregation, in review. (2012)

# Effect of Oxygen Dispersion Flow Rate



Increasing  $O_2$  flow rate results in a shorter residence time at high temperatures<sup>1</sup>

1. S.E. Pratsinis, W.H. Zhu & S. Vemury, Powder Technol. 86 (1996) 87-93.

# Summary & Conclusions

- Mass-mobility relation in free molecular and transition regime:

$$d_{va} = \left( \frac{\pi k_a}{6\nu} (d_m)^{2D_\alpha} \right)^{1/(2D_\alpha - 3)}$$

- independent of time, material or sintering mechanism, with  $k_a = 1.0$  &  $D_\alpha = 1.07$
- The  $d_{va}$  by online mass-mobility measurements is in good agreement with ex-situ BET & TEM measurements.



Thank you for your attention

Creux du Van, Neuchatel, August 22, 2011



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Prof. Hans J. Herrmann, ETH Zürich

Arto Gröhn, ETH Zürich

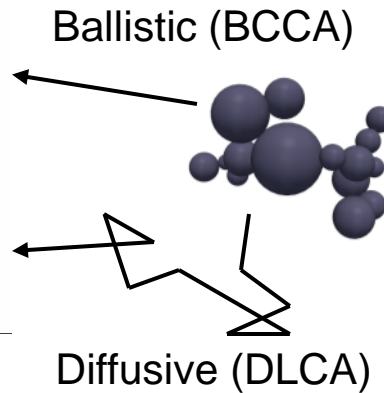
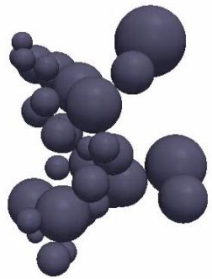
Dr. Dirk Kadau, Wärtsilä Schweiz AG

Dr. Frank Krumeich, ETH Zürich

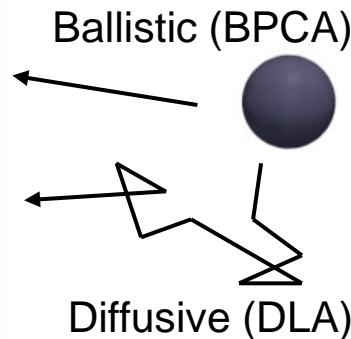
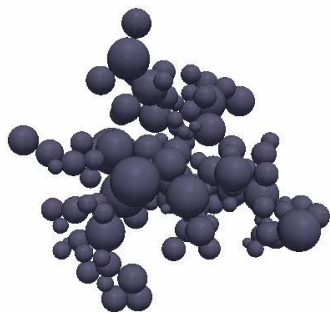


# Agglomerates of Polydisperse Primary Particles (PP)

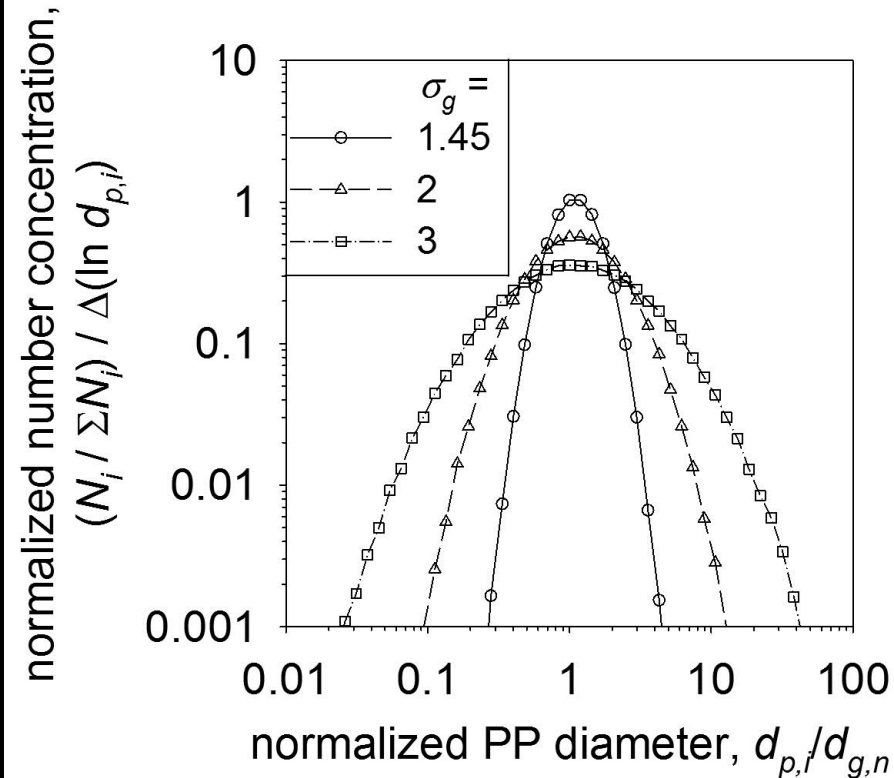
by cluster-cluster agglomeration<sup>1</sup>:



by particle-cluster agglomeration<sup>2</sup>:



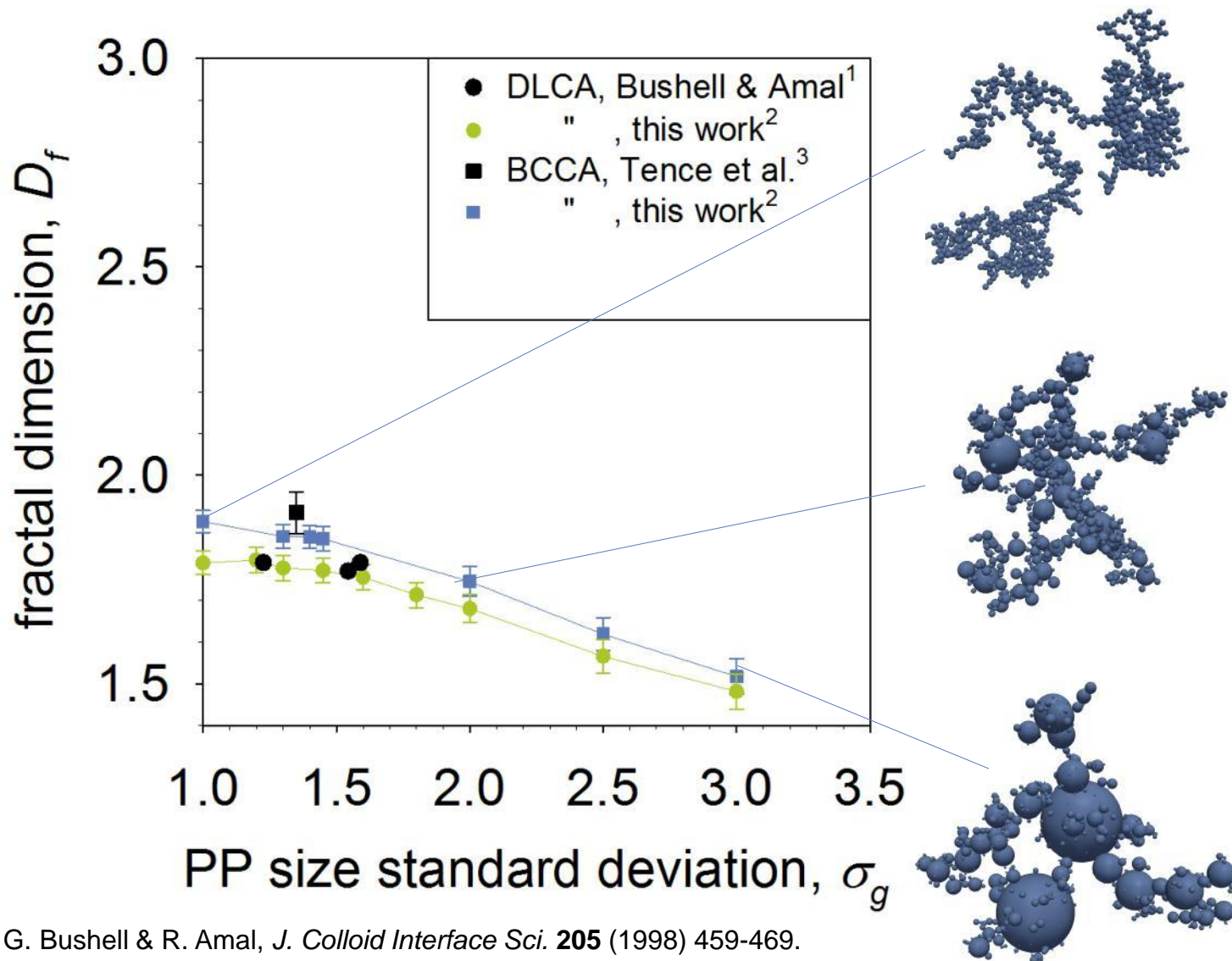
Log-normal PP distribution



1. R. Botet, R. Jullien & M. Kolb, *J. Phys. A: Math. Gen.* **17** (1984) L75-L79.

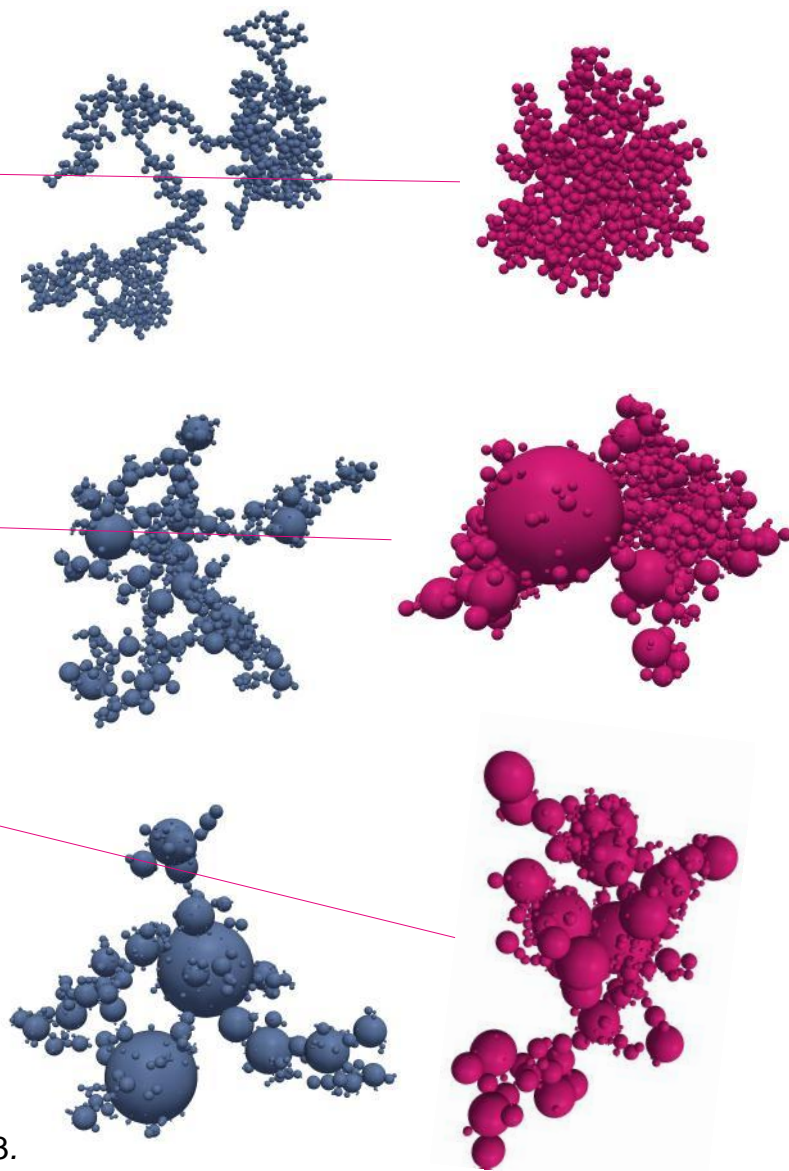
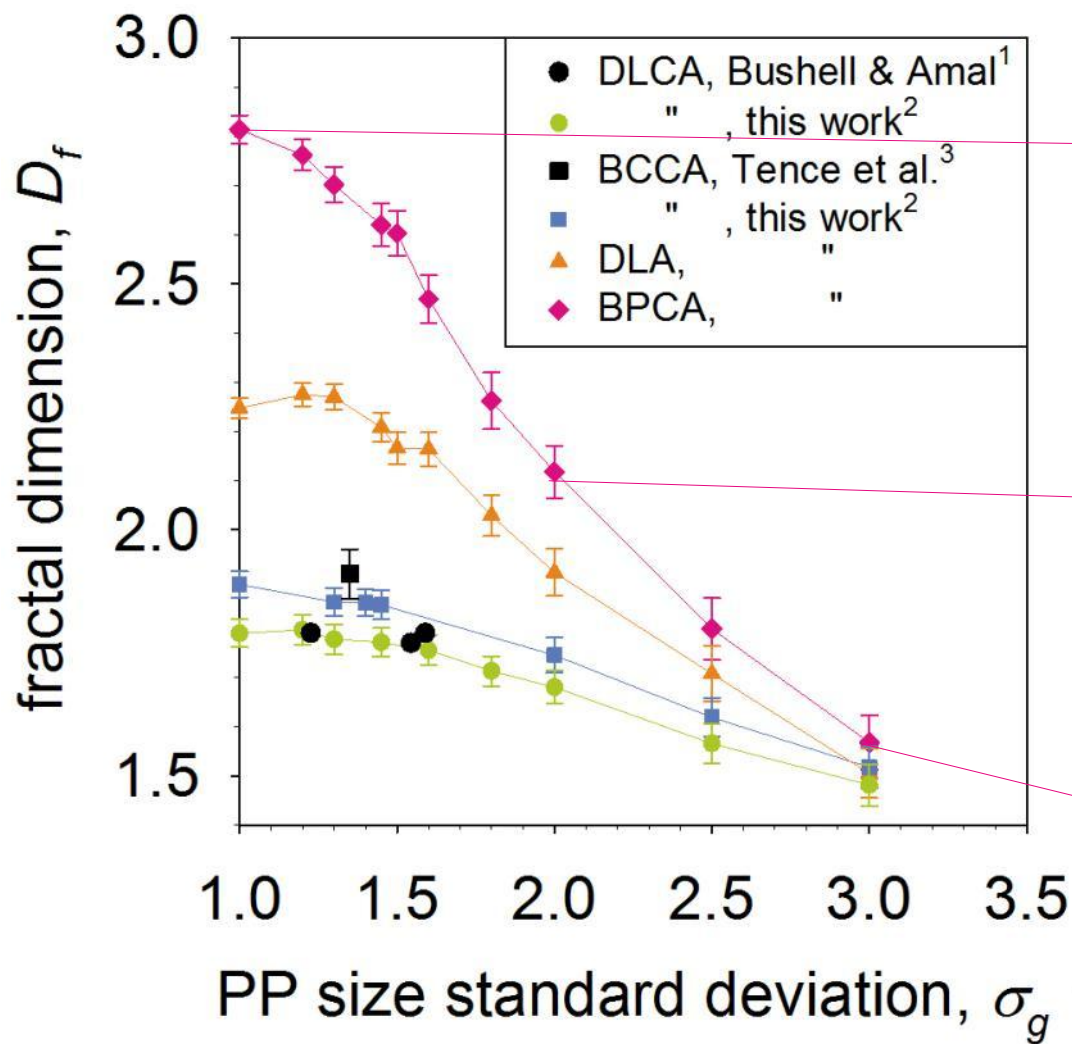
2. T.A. Witten & L.M. Sander, *Phys. Rev. Lett.* **47** (1981) 1400-1403.

# Effect of PP Polydispersity on $D_f$



1. G. Bushell & R. Amal, *J. Colloid Interface Sci.* **205** (1998) 459-469.
2. M.L. Eggersdorfer & S.E. Pratsinis, *Aerosol Sci. Technol.* **46** (2012) 347-353.
3. M. Tence, J.P. Chevalier & R. Jullien, *J. Phys.* **47** (1986) 1989-1998.

# Effect of PP Polydispersity on $D_f$

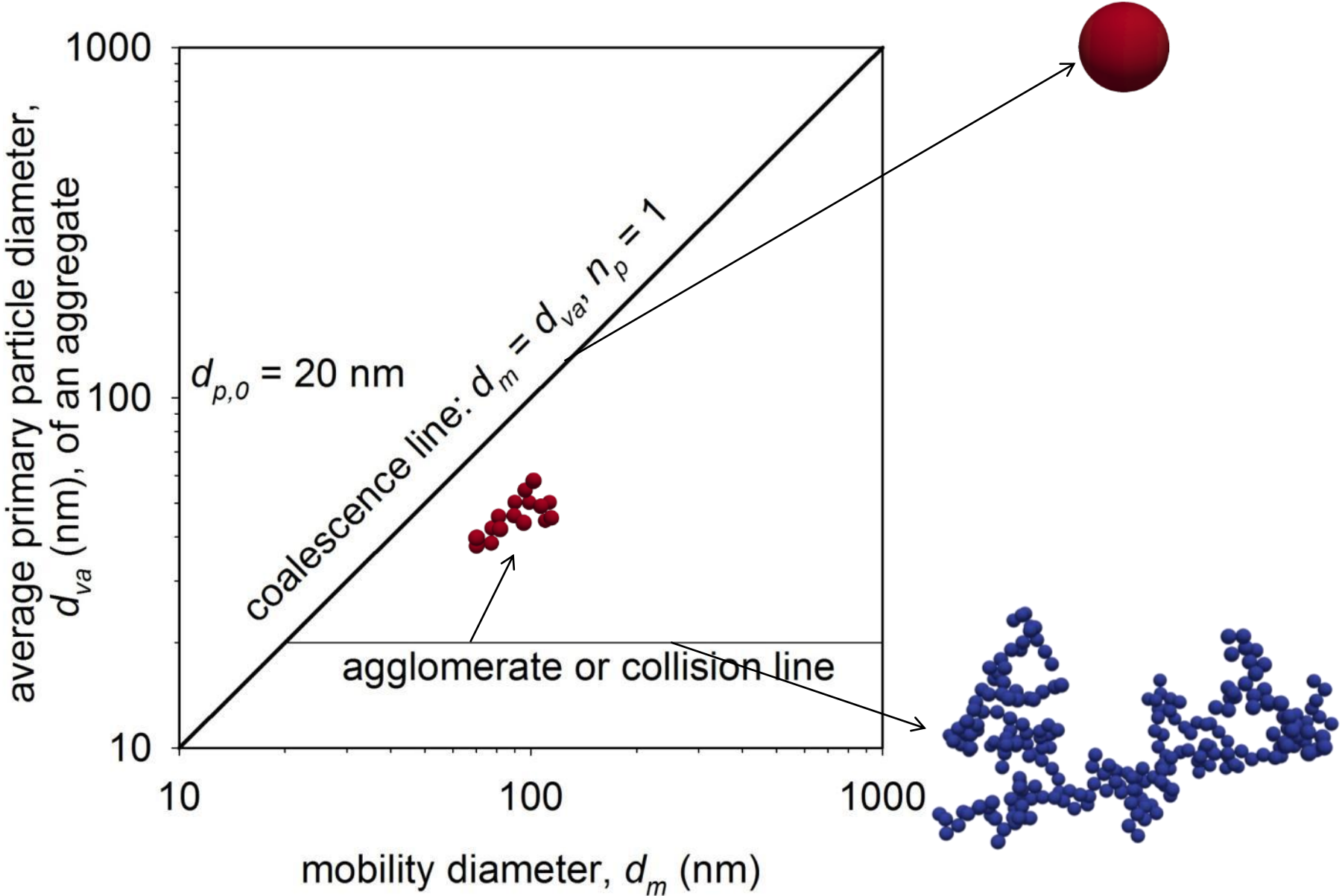


1. G. Bushell & R. Amal, *J. Colloid Interface Sci.* **205** (1998) 459-469.
2. M.L. Eggersdorfer & S.E. Pratsinis, *Aerosol Sci. Technol.* **46** (2012) 347-353.
3. M. Tence, J.P. Chevalier & R. Jullien, *J. Phys.* **47** (1986) 1989-1998.

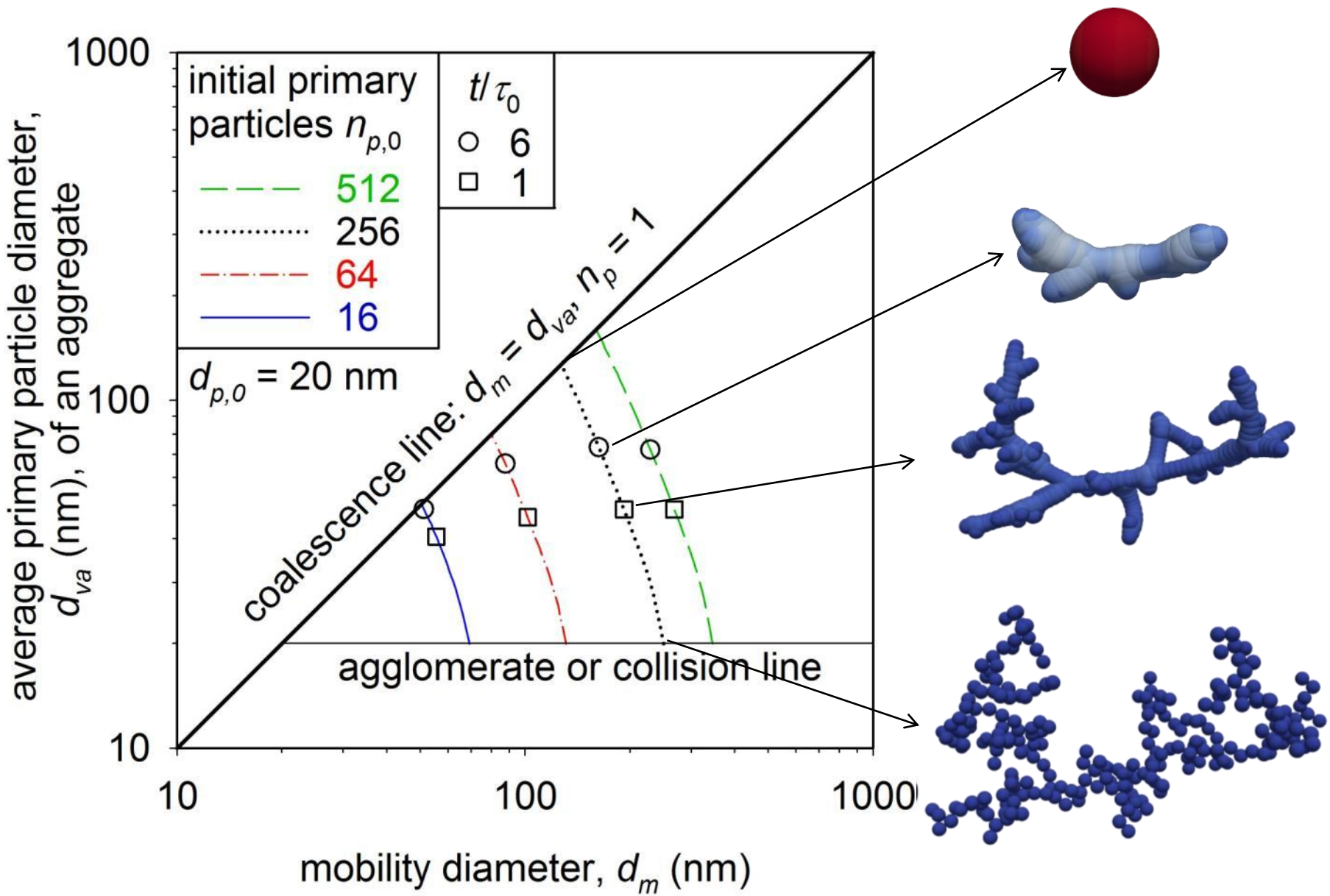
# Summary & Conclusions

- PP Polydispersity reduces  $D_f$  &  $D_{fm}$  and determines agglomerate structure for large  $\sigma_g$  ( $> 2.5$ )

# Mobility $d_m$ & Primary Particle Diameter $d_{va}$ during Sintering



# Mobility $d_m$ & Primary Particle Diameter $d_{va}$ during Sintering





# Application to Silver Nanoparticle Sintering<sup>1</sup>

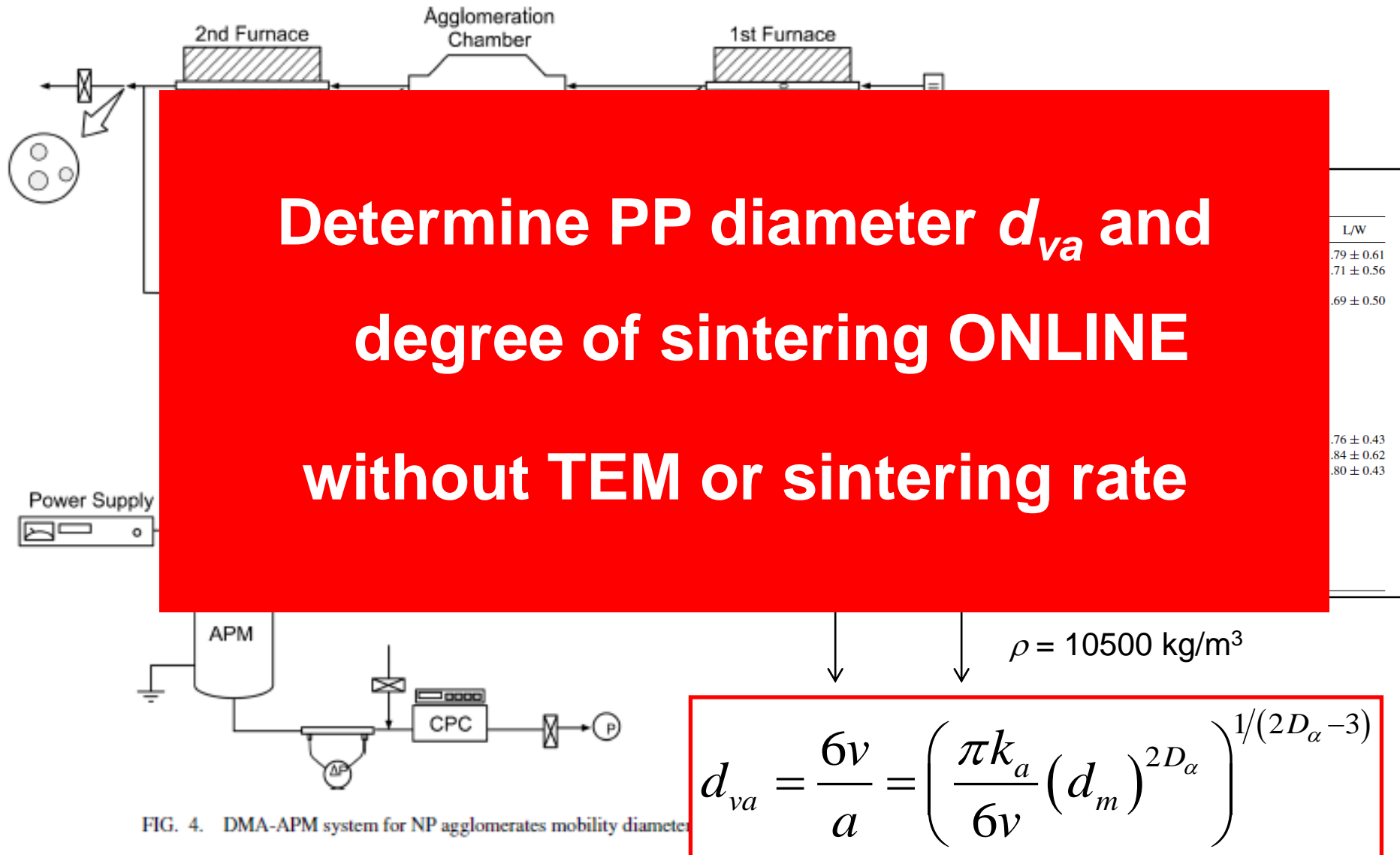
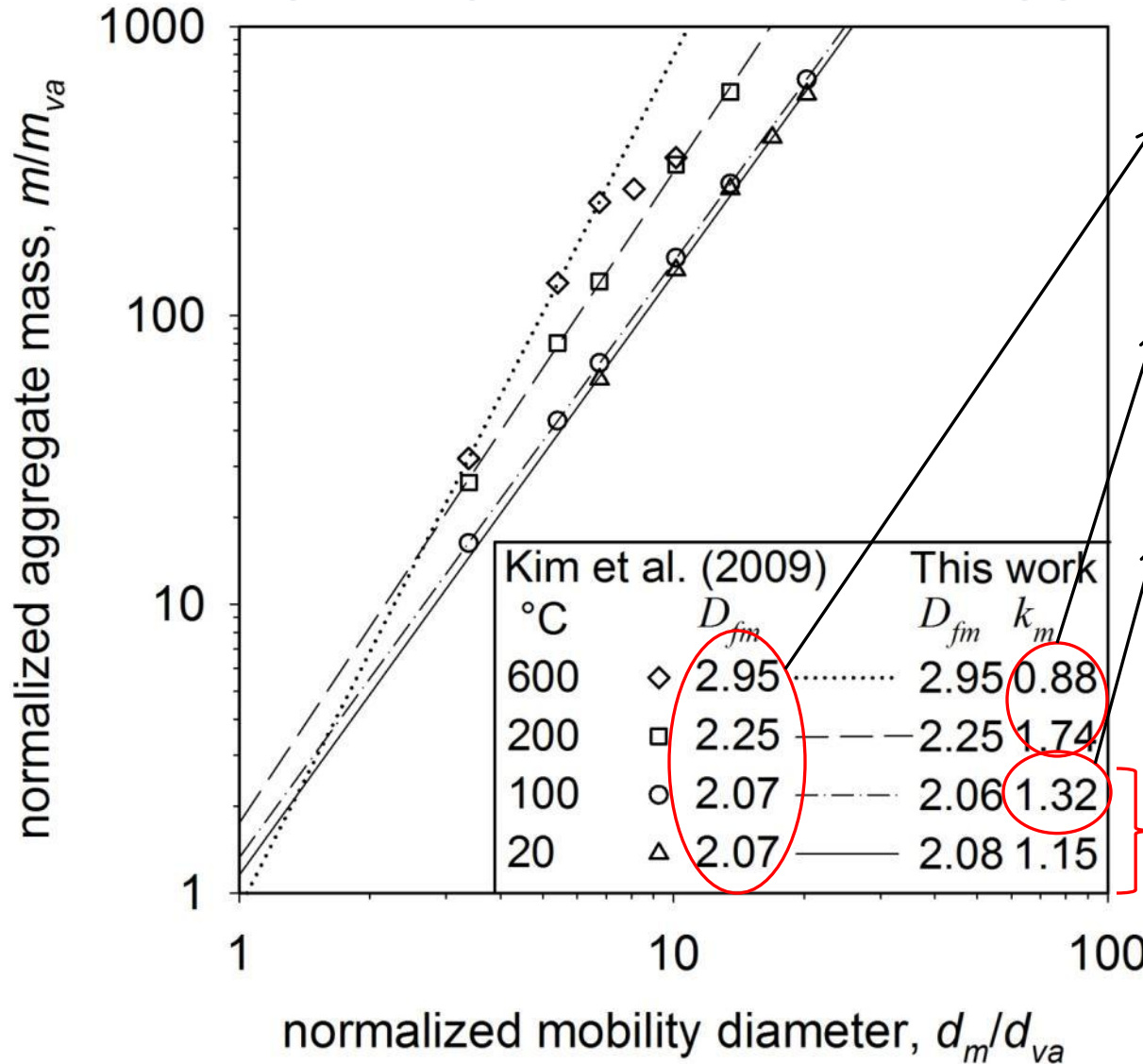


FIG. 4. DMA-APM system for NP agglomerates mobility diameter

1. S.C. Kim, J. Wang, M.S. Emery, W.G. Shin, G.W. Mulholland & D.Y.H. Pui, *J. Aerosol Sci.* **43** (2009) 344-355.

# Comparison to Experiments<sup>1</sup>: Sintering of Ag – Nanoparticle Aggregates



Monotonic increase  
in  $D_{fm}$

A maximum in  $k_m$  is  
reached

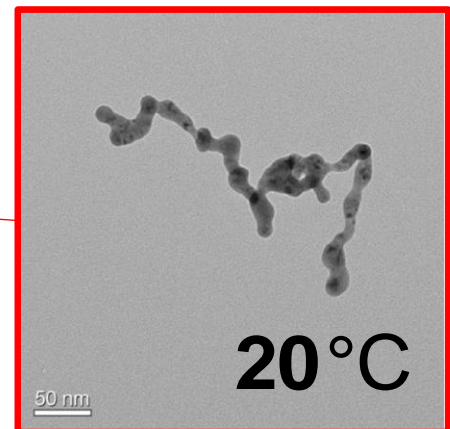
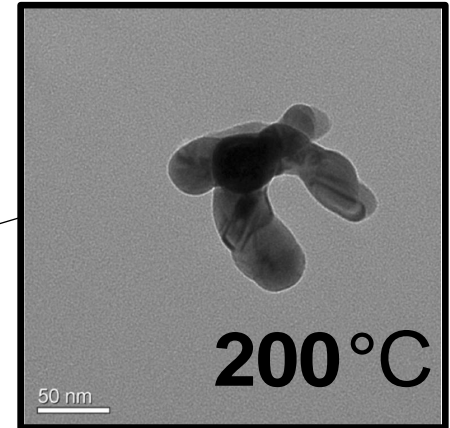
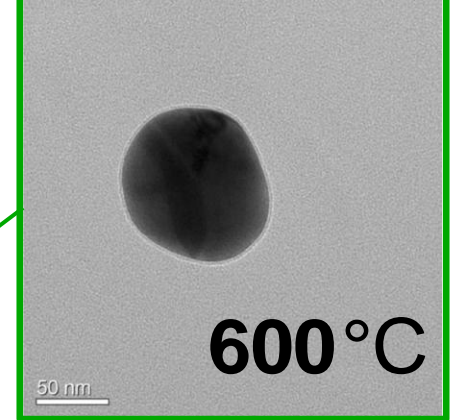
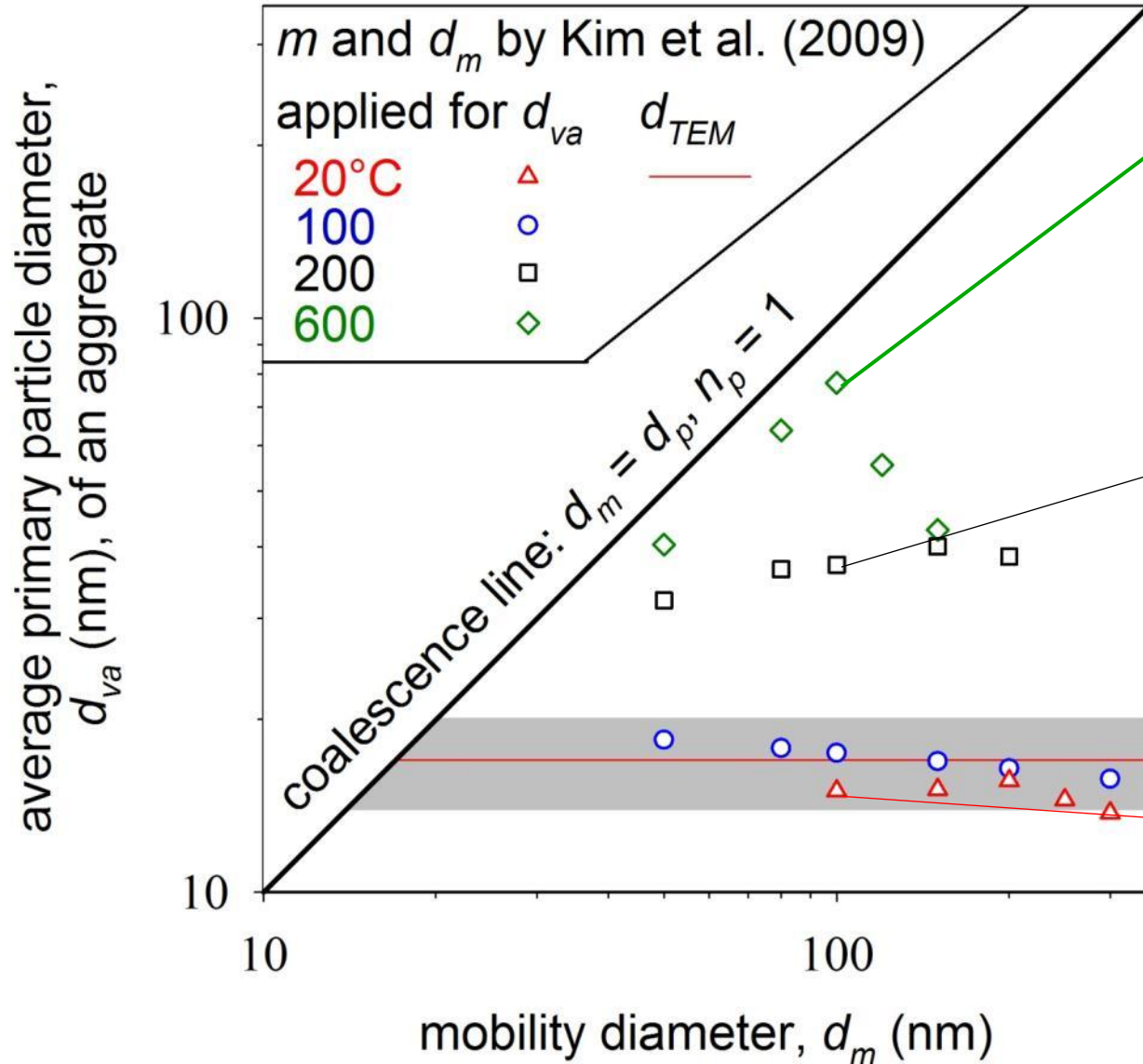
Increase in prefactor  
 $k_m$  is indication for  
sinter neck formation

Close to theoretical  
value of  $D_{fm} = 2.15$  for  
DLCA<sup>2</sup>

1. S.C. Kim, J. Wang, M.S. Emery, W.G. Shin, G.W. Mulholland & D.Y.H. Pui, *J. Aerosol Sci.* **43** (2009) 344-355.

2. C.M. Sorensen, *Aerosol Sci. Technol.* **45** (2011) 755-769.

# Application to Experiments<sup>1</sup>: Sintering of Ag – Nanoparticle Aggregates

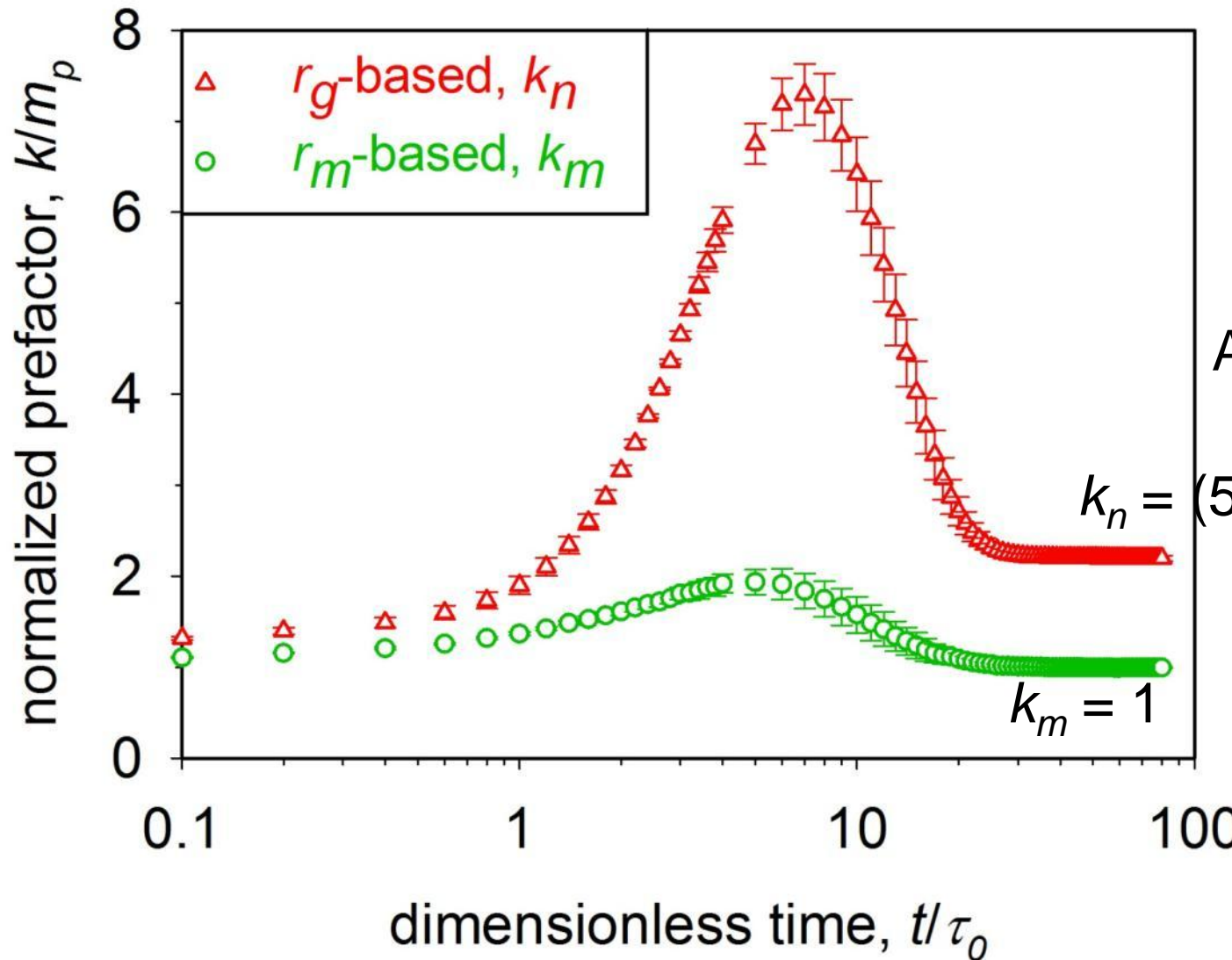


1. S.C. Kim, J. Wang, M.S. Emery, W.G. Shin, G.W. Mulholland & D.Y.H. Pui, *J. Aerosol Sci.* **43** (2009) 344-355.

# Evolution of Prefactors $k_n$ & $k_m$

$$\frac{m}{m_p} = k_n \left( \frac{r_g}{r_p} \right)^{D_f}$$

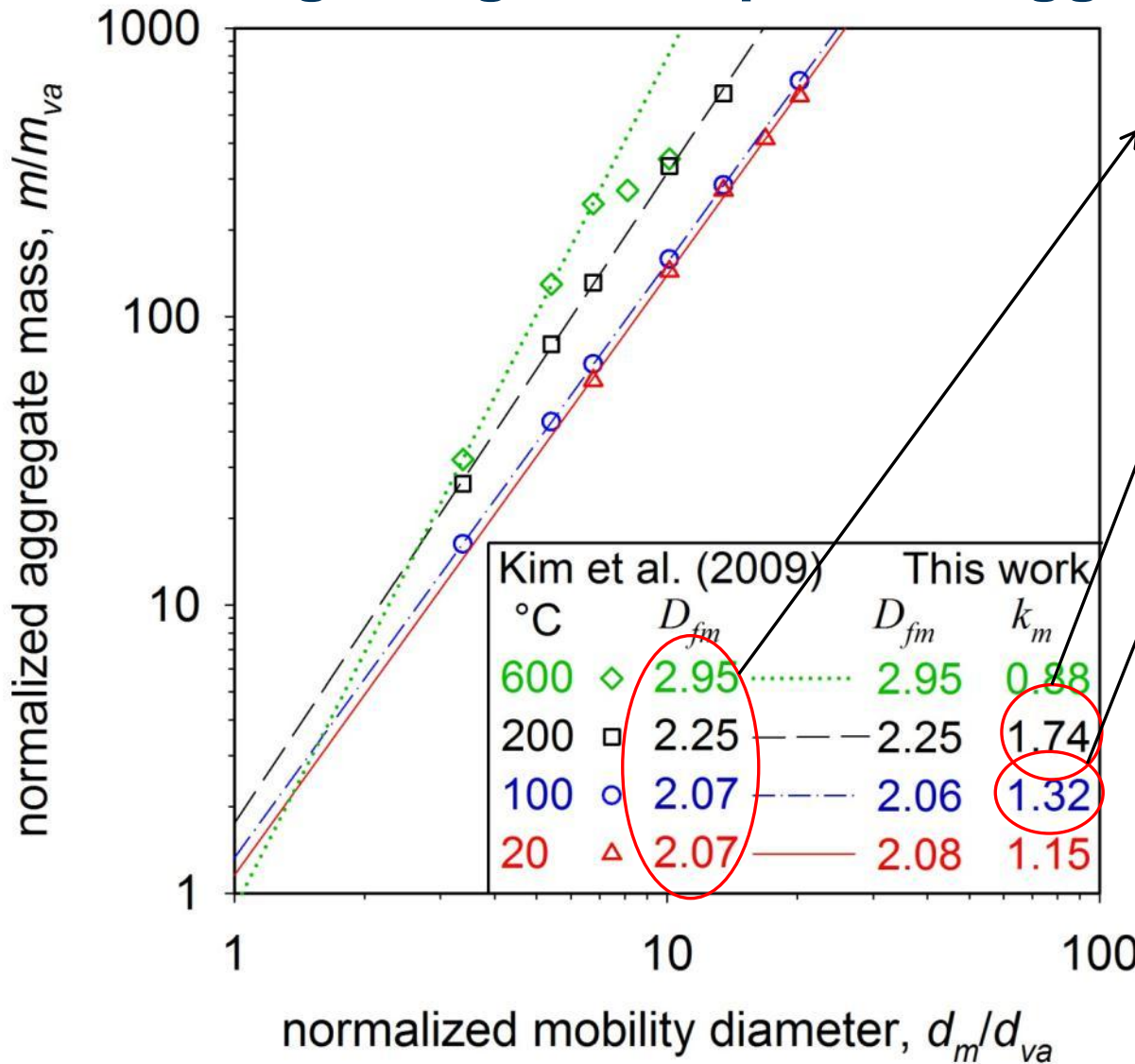
$$\frac{m}{m_p} = k_m \left( \frac{r_m}{r_p} \right)^{D_{fm}}$$



Asymptotic values

Both  $k_n$  and  $k_m$  reach a maximum

# Comparison to Experiments<sup>1</sup>: Sintering of Ag – Nanoparticle Aggregates



Monotonic increase  
in  $D_{fm}$

A maximum in  $k_m$  is  
reached

Increase in prefactor  
 $k_m$  is indication for  
sinter neck formation

Close to theoretical  
value of  $D_{fm} = 2.15$  for  
DLCA<sup>2</sup>

1. S.C. Kim, J. Wang, M.S. Emery, W.G. Shin, G.W. Mulholland & D.Y.H. Pui, *J. Aerosol Sci.* **43** (2009) 344-355.

2. C.M. Sorensen, *Aerosol Sci. Technol.* **45** (2011) 755-769.

# Summary and Conclusions I

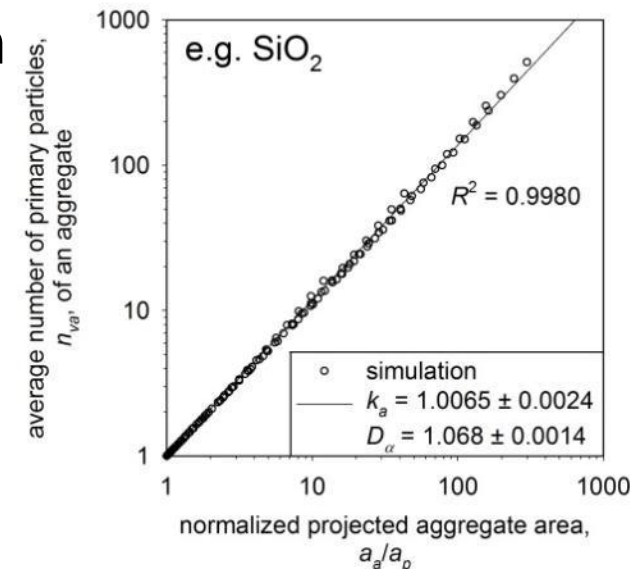
1. We propose a formula to calculate  $d_{va}$  for nanoparticle agglomerates/aggregates/spheres.

$$d_{va} = \frac{6\nu}{a} = \left( \frac{\pi k_a}{6\nu} (d_m)^{2D_\alpha} \right)^{1/(2D_\alpha - 3)}$$

2. Viscous flow<sup>1</sup> and grain boundary diffusion sintering simulations show that

$$n_{va} = k_a \left( \frac{a_a}{a_{va}} \right)^{D_\alpha}$$

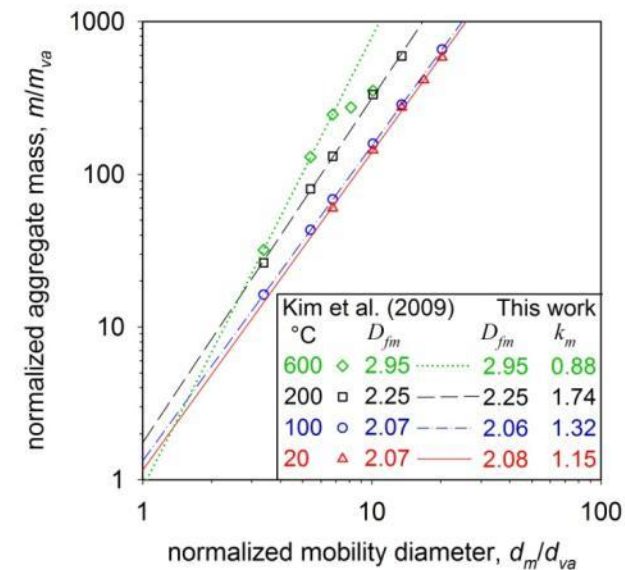
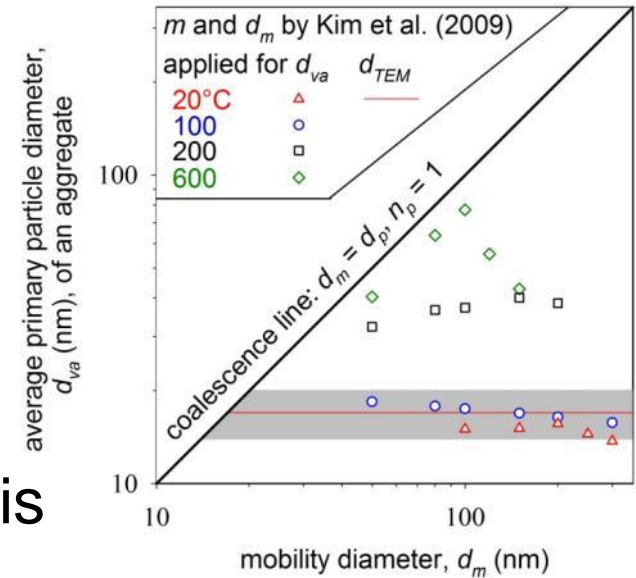
is valid during sintering  $\rightarrow D_\alpha$  &  $k_a$ .

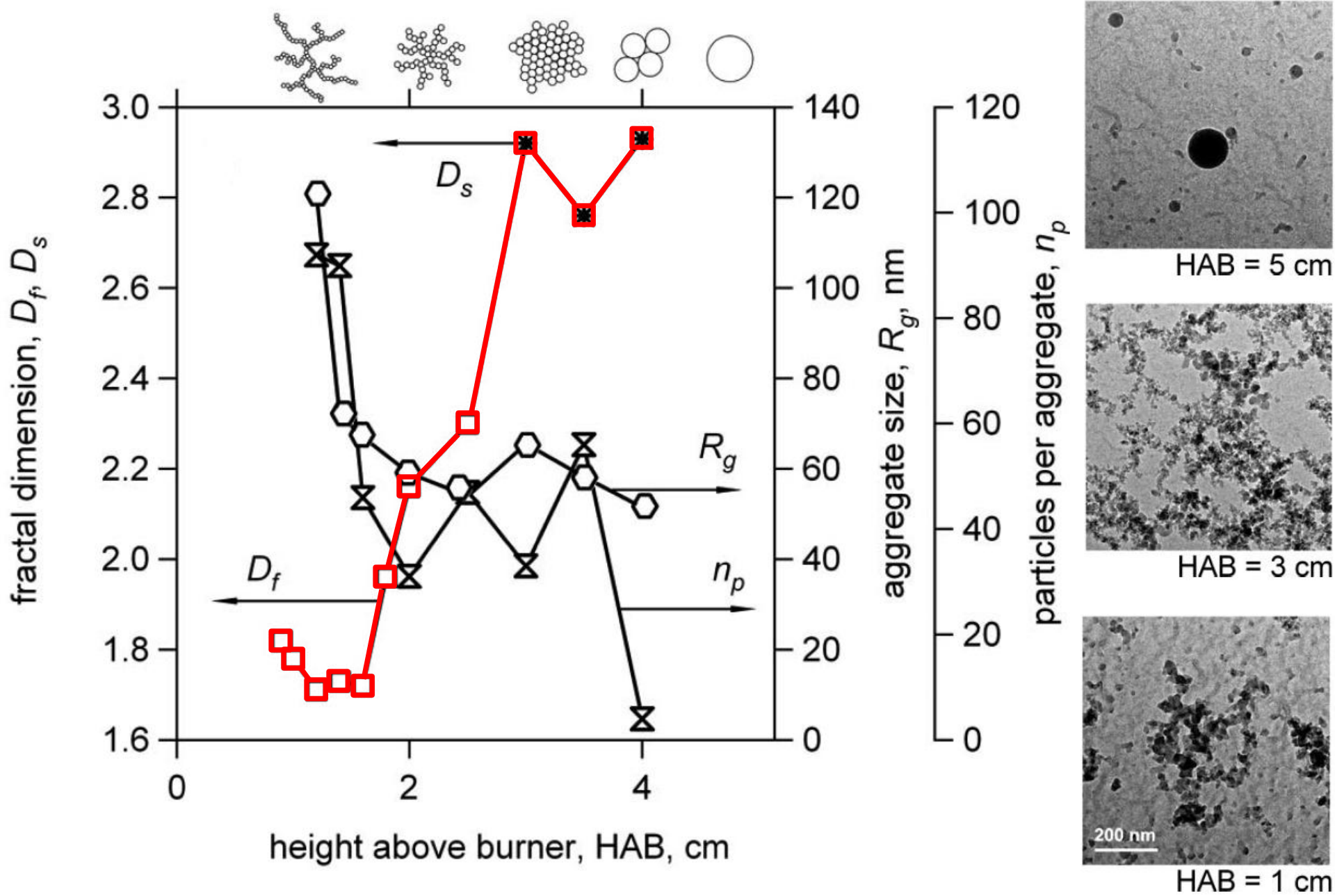


1. M.L. Eggersdorfer, D. Kadau, H.J. Herrmann & S.E. Pratsinis, *Langmuir* **27** (2011) 6358-6367.

# Summary and Conclusions II

- $d_{va}$  &  $n_{va}$  can be determined by realtime mass-mobility (e.g. DMA-APM) measurements using  $D_\alpha$  &  $k_a$  from simulations.
- Good agreement between  $d_{va}$  and  $d_{TEM}$  is found.
- The extent of sintering is best described by mass-mobility exponent  $D_{fm}$  (monotonic increase).
- Increase in prefactor  $k_m$  is an indication for sinter neck formation.

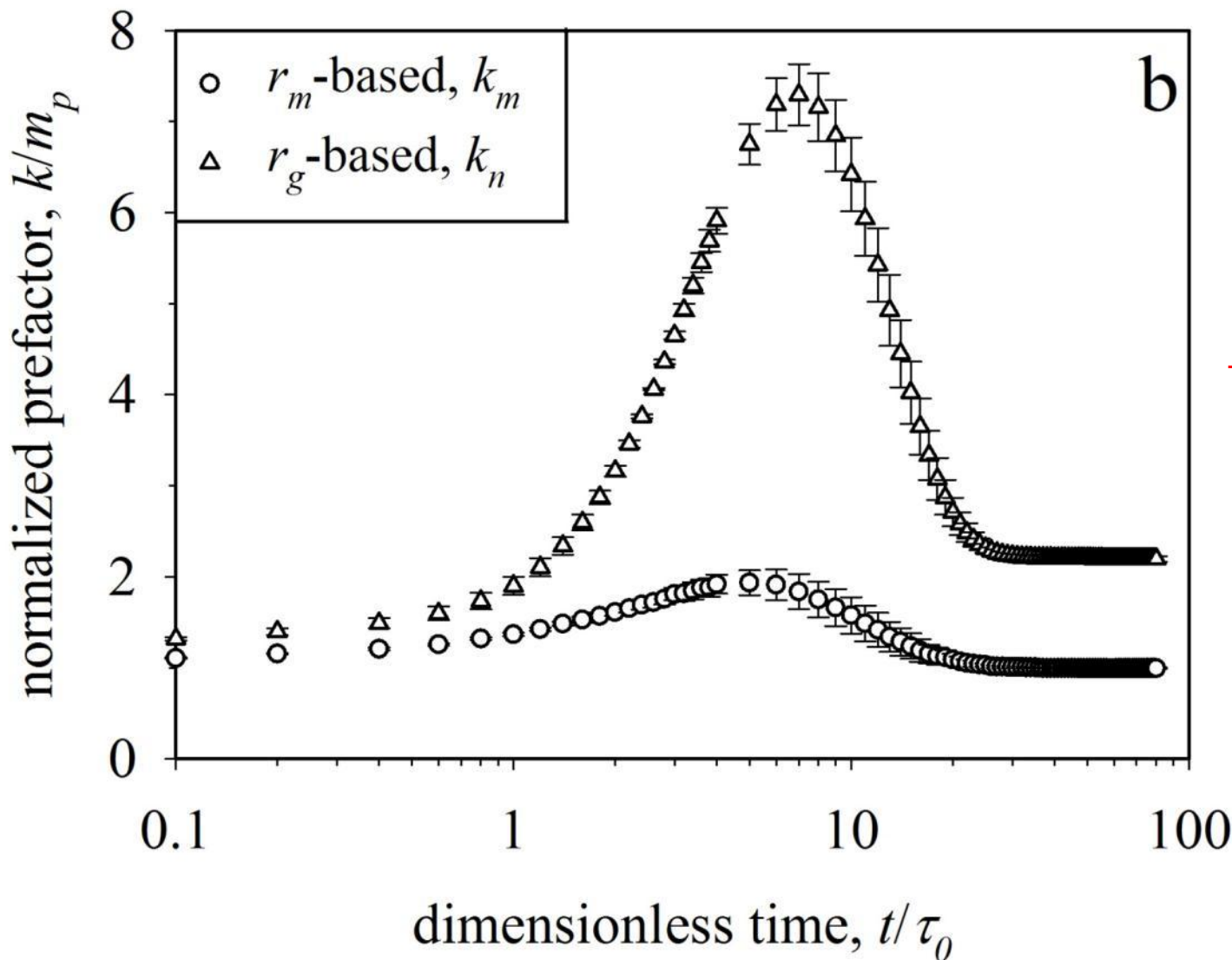




A. Camenzind, H. Schulz, A. Teleki, G. Beaucage, T. Narayanan & S.E. Pratsinis, *Eur. J. Inorg. Chem.* (2008) 911-918.



# Evolution of Prefactor $k_n$ and $k_m$ during Sintering

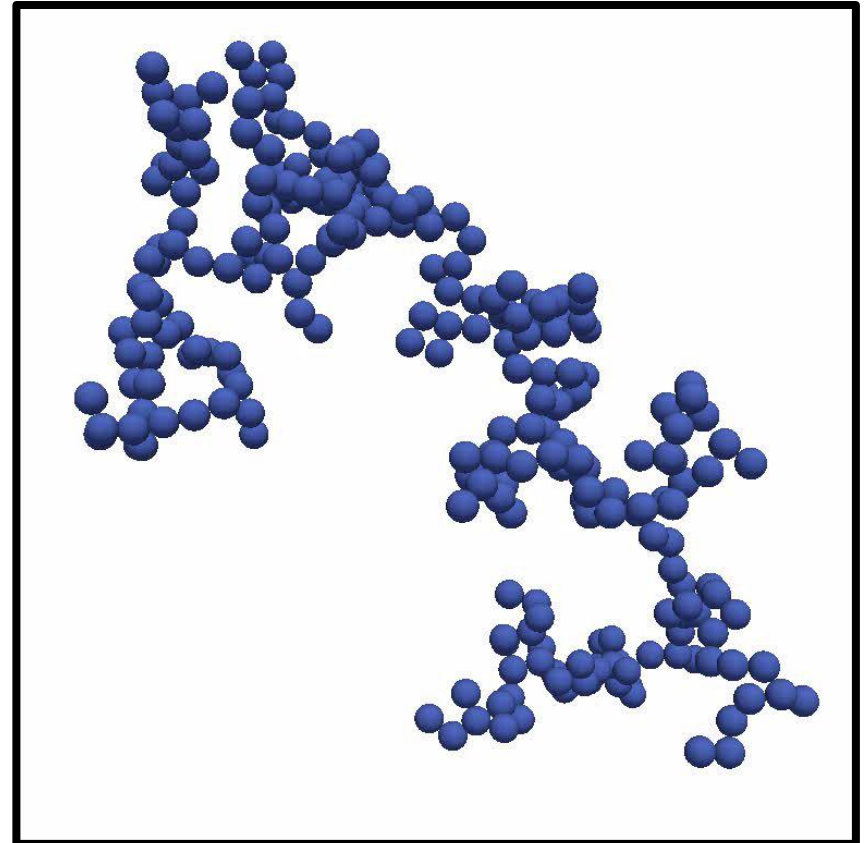


$$\frac{m}{m_p} = k_n \left( \frac{r_g}{r_p} \right)^{D_f}$$

$$\frac{m}{m_p} = k_m \left( \frac{r_m}{r_p} \right)^{D_{fm}}$$

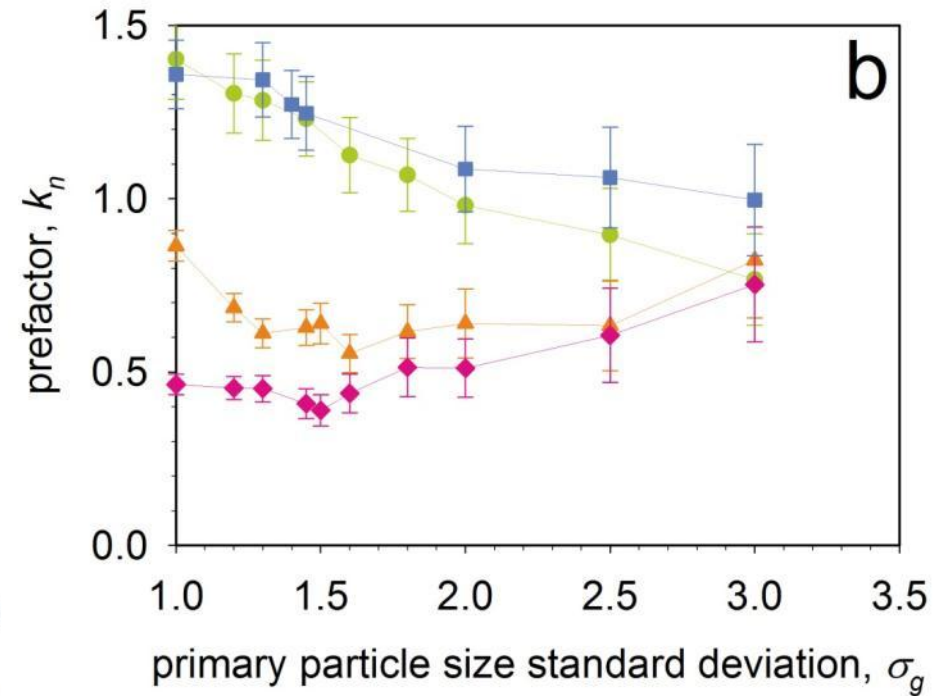
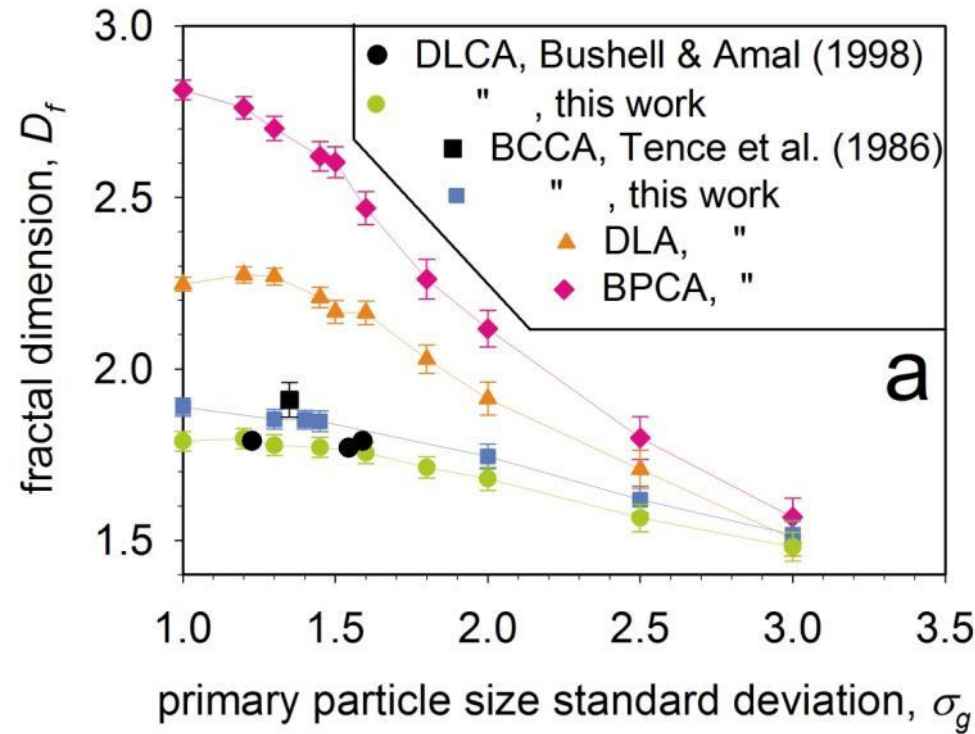
# Simulation Method: Multi-Particle Sintering

- Color: particle size based on curvature
- Vorlume<sup>1</sup> software to calculate particle volume, surface and neck area.
- SHAKE<sup>2</sup> algorithm to fulfill constraints for particle distances.
- Simulate viscous sintering of aggregates:
  - $N = 2 - 512$  primary particles
  - Average over 50 aggregates of each size (irregular structures)

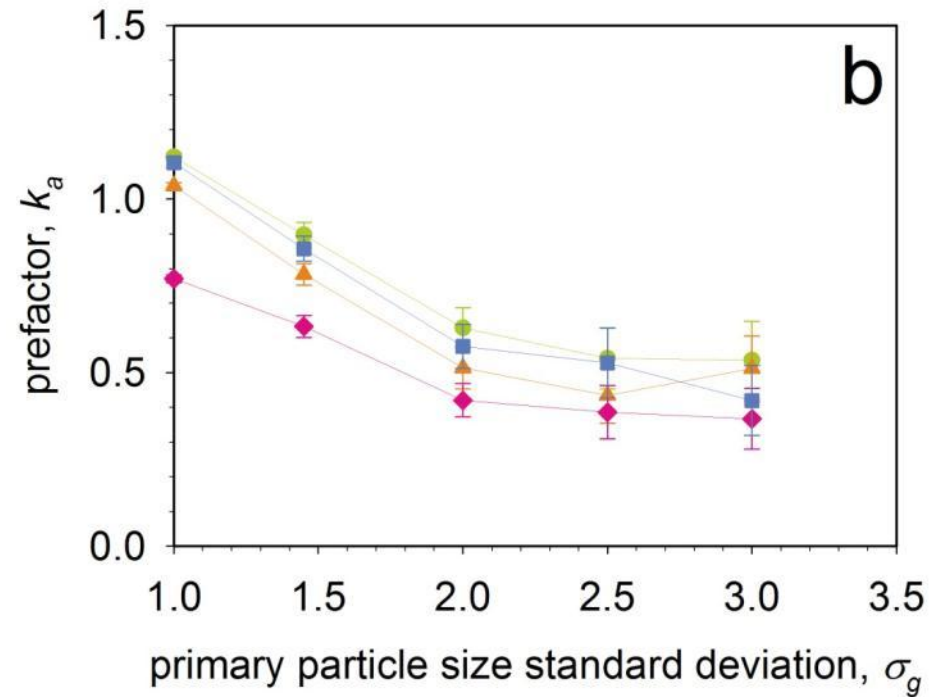
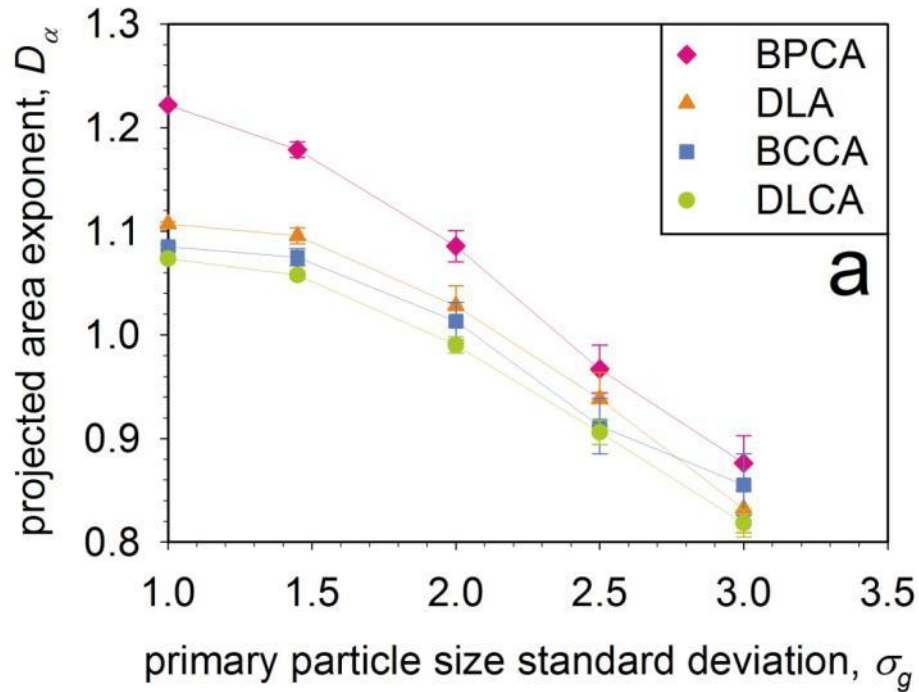


1. F. Cazals, H. Kanhere & S. Lorient, *INRIA Tech Report No. 7013* (2009).  
2. J.P. Ryckaert, G. Ciccotti & H.J.C. Berendsen, *J. Comp. Phys.* **23** (1977) 327-341.

# Effect of Primary Particle Polydispersity on $D_f$ and $k_n$

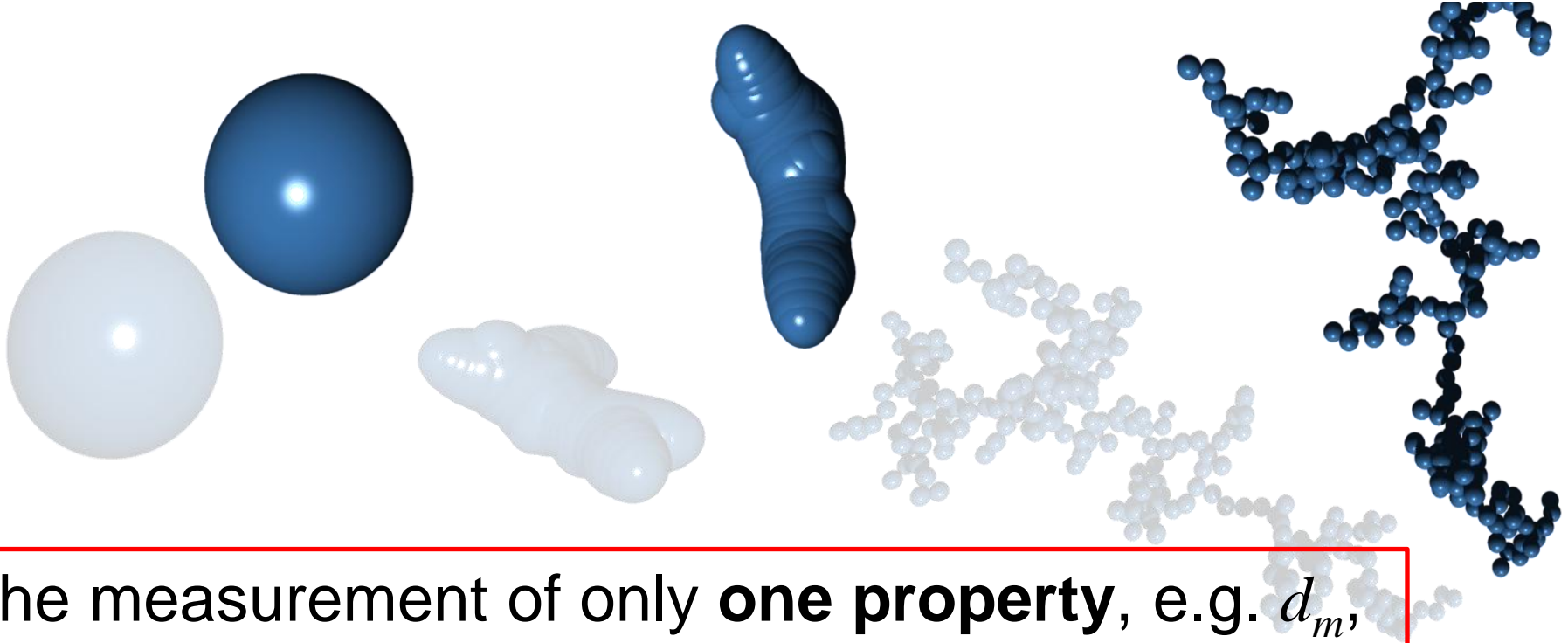


# Effect of Primary Particle Polydispersity on $D_\alpha$ and $k_a$



# Goal: Online Characterization of Nanoparticle Morphology

Mobility size<sup>1,2</sup>  $d_m$ :  $d_{m,1} = d_{m,2} = d_{m,3} \rightarrow$  e.g. DMA  
Mass  $m$ :  $m_1 > m_2 > m_3 \rightarrow$  e.g. APM  
Surface area  $a$ :  $a_1 < a_2 < a_3 \rightarrow$  e.g. UNPA

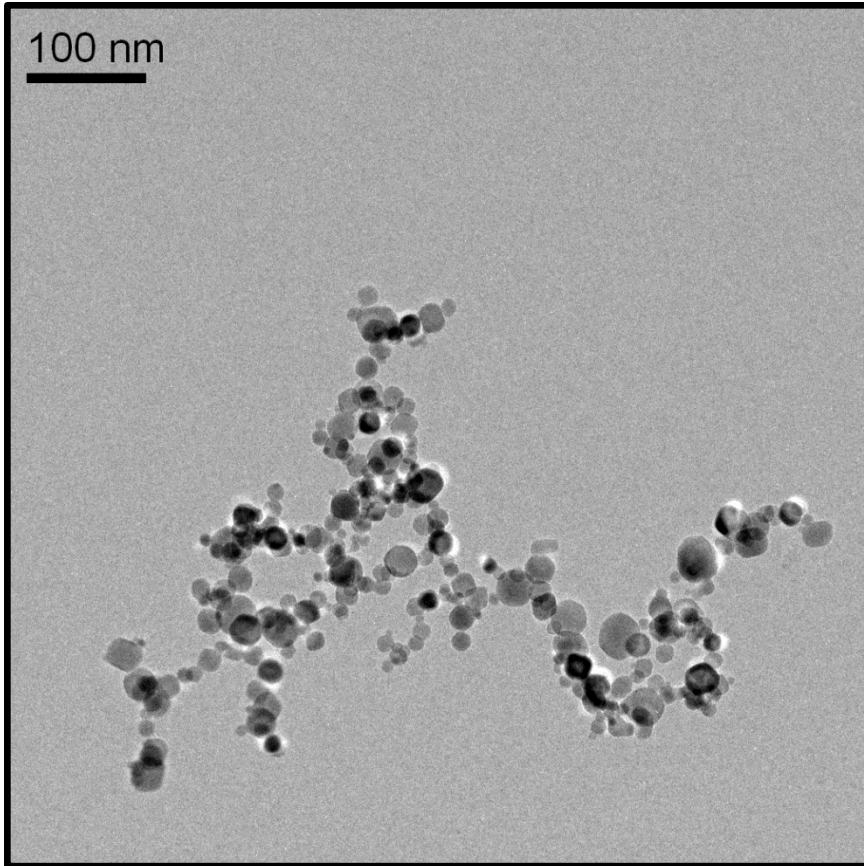


The measurement of only **one property**, e.g.  $d_m$ ,  
is **not sufficient** to characterize aggregate/  
agglomerate structure

1. P. Meakin, *Adv. Colloid Interface Sci.* **28** (1988) 249-331.
2. S.N. Rogak, R.C. Flagan & H.V. Nguyen, *Aerosol Sci. Technol.* **18** (1993) 25-47.

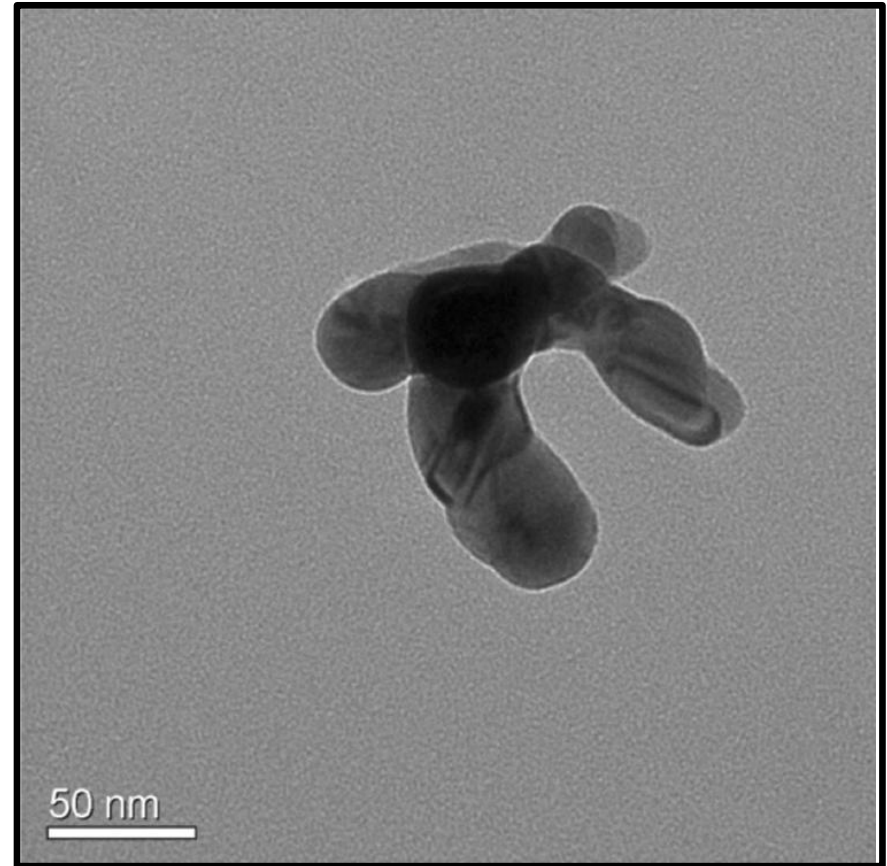
# Nomenclature

agglomerate:  
physically bonded



ZrO<sub>2</sub> agglomerate generated by FSP @ PTL, ETH Zürich

aggregate:  
chemically or sinter-bonded



S.C. Kim, J. Wang, M.S. Emery, W.G. Shin, G.W. Mulholland & D.Y.H. Pui, *J. Aerosol Sci.* **43** (2009) 344-355.